

An Overview of Flow Regimes
Describing Slurry Transport

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Safety Moment

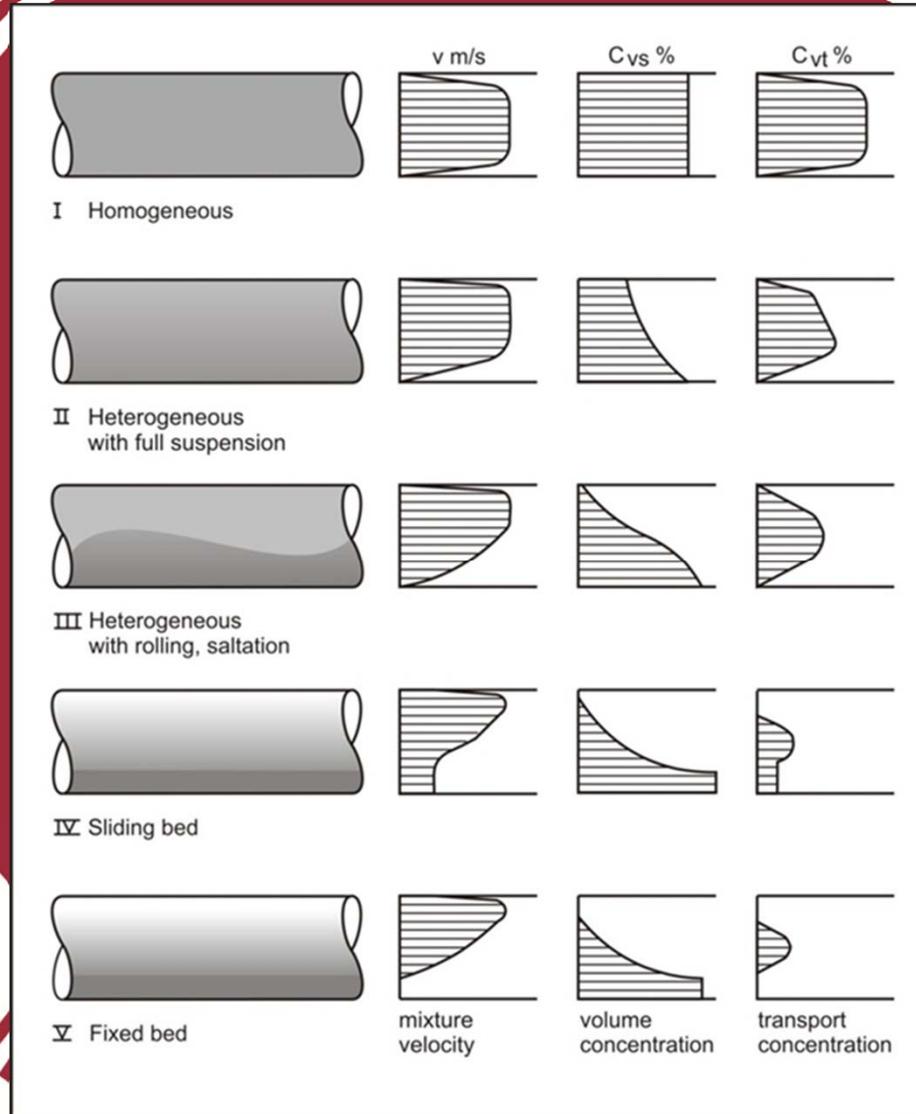




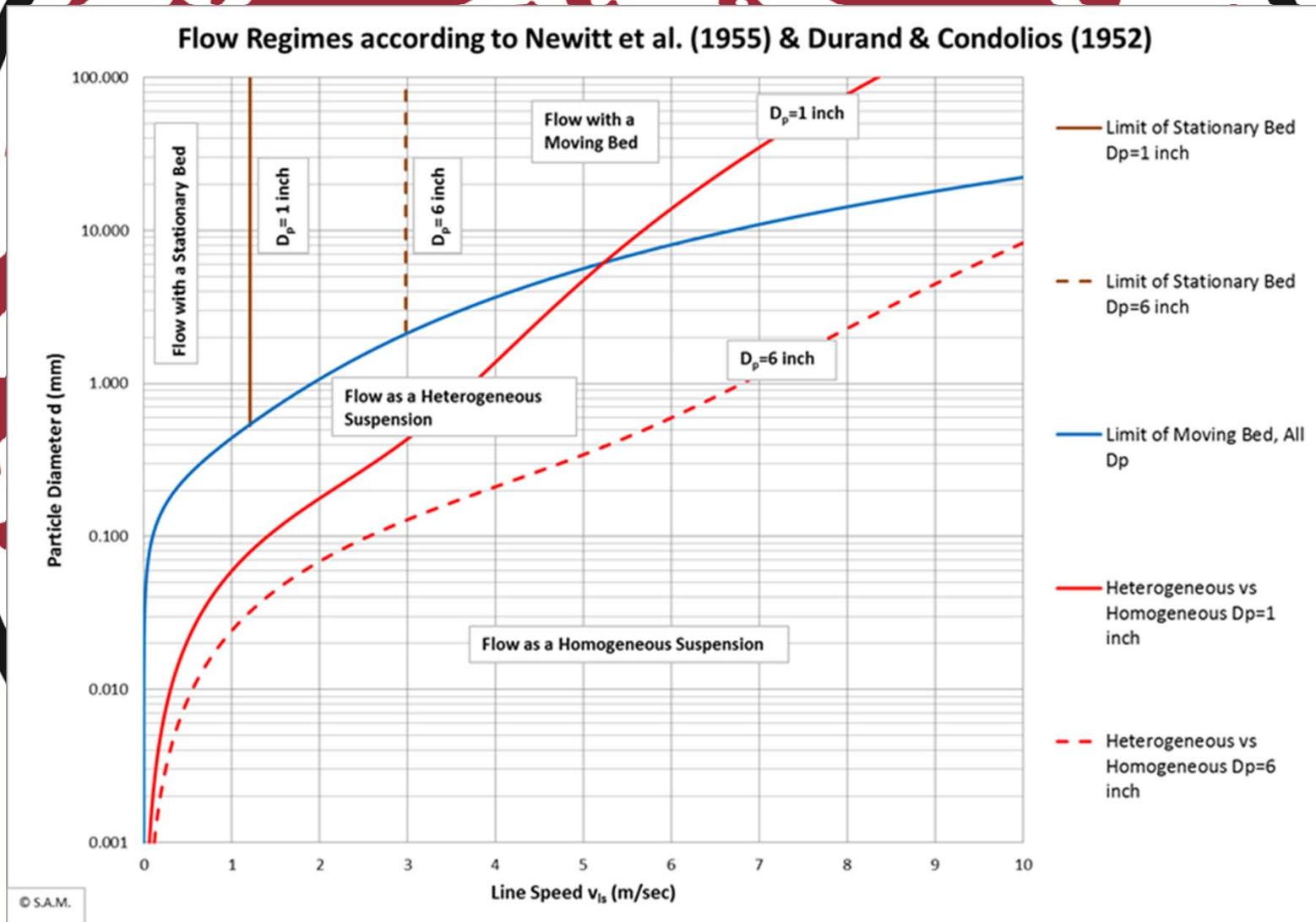
Problem Definition

- There are many models, empirical and fundamental for the various phases of flow
- The models are often based on lab tests, and often in small pipe relative to current dredging practice
- There is still no generic fundamental model for slurry transport, particularly in large diameter pipelines, connecting the different flow regimes

Regimes History

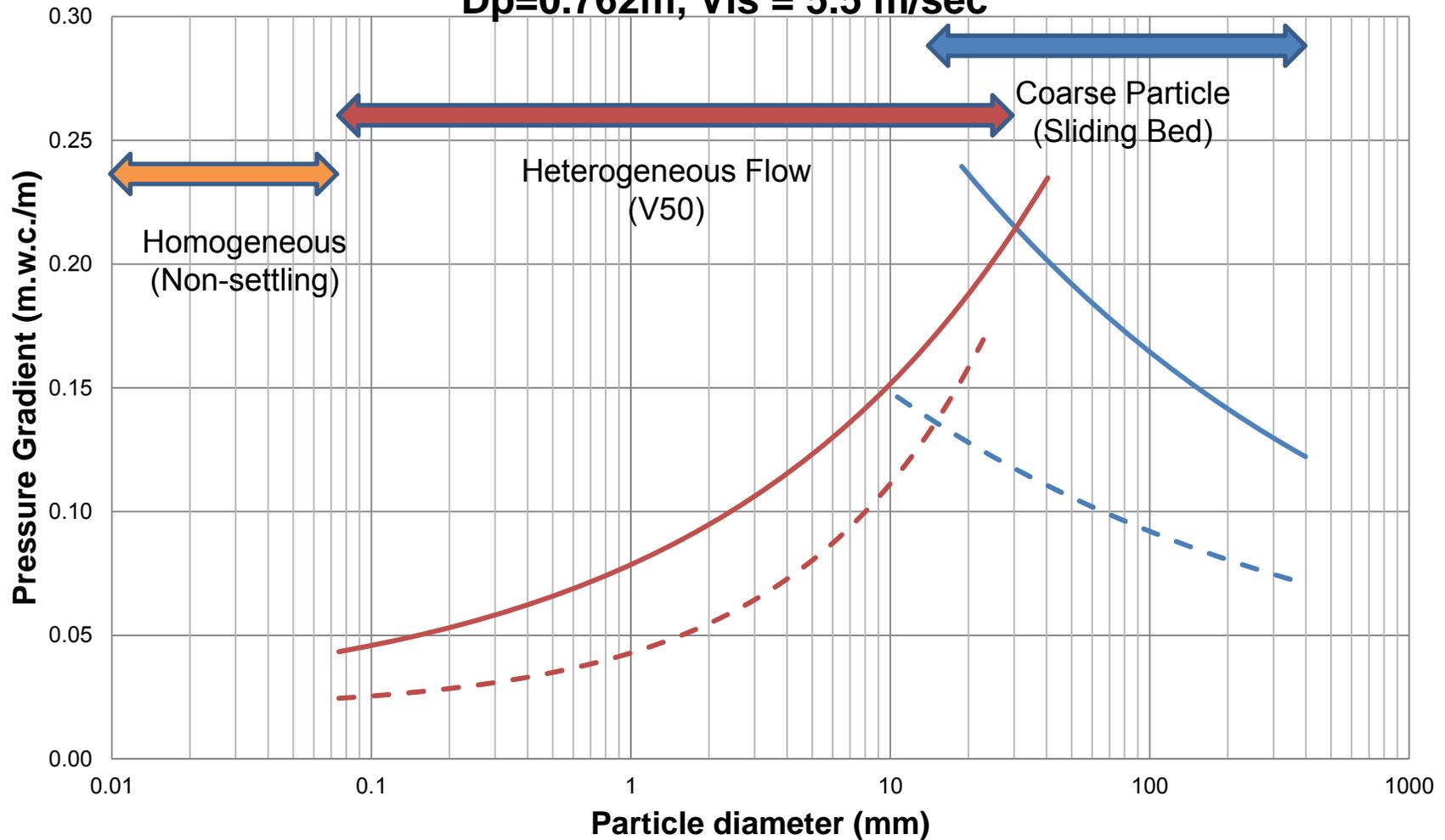


Newitt et al. (1955) D, C & G (1952, 1960)



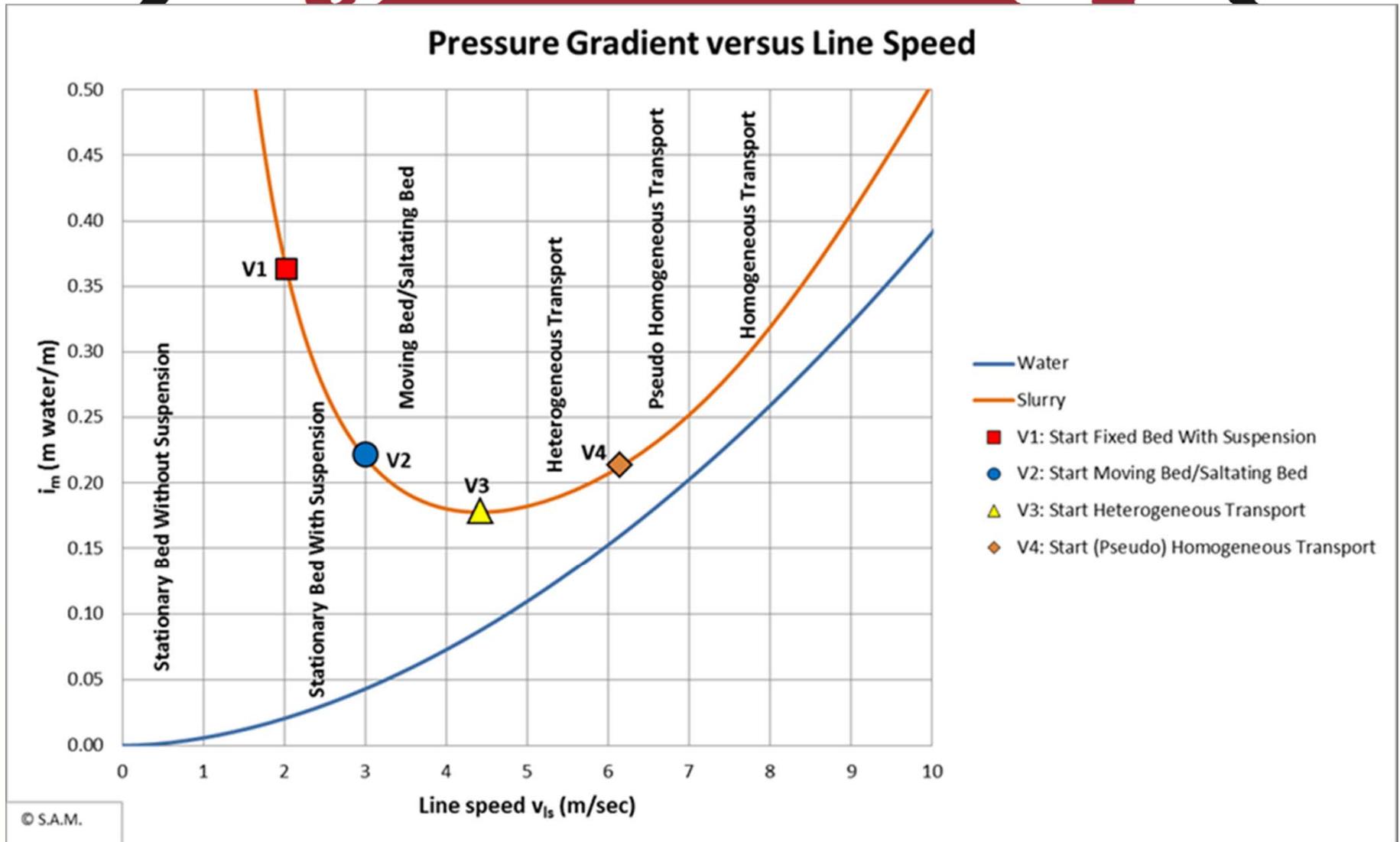
Wilson, Addie, Sellgren & Clift (1992)

Comparison of Transport Models
 $D_p=0.762\text{m}$, $V_{Is} = 5.5 \text{ m/sec}$



IMPROVEMENTS

Abulnaga (2002)



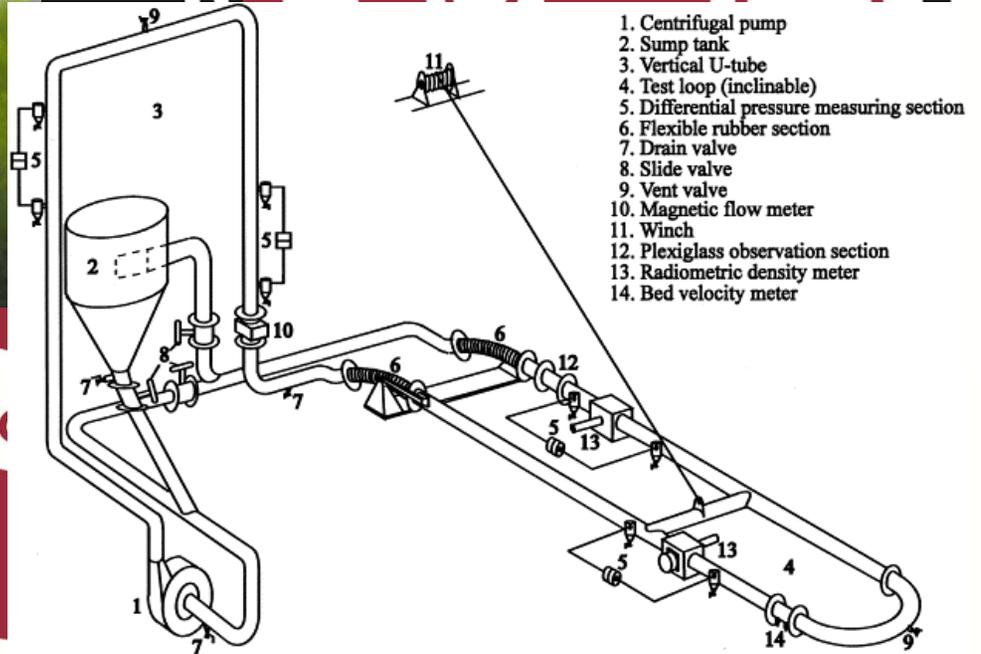
9 Flow Regimes



Volume Concentrations

$$C_v = \frac{\rho_m - \rho_{fl}}{\rho_s - \rho_{fl}} : \text{Volume concentration from density readings}$$

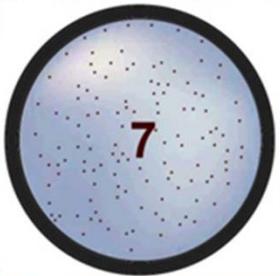
$$C_{vt} = \frac{\dot{v}_s}{\dot{v}_m} : \text{Transport (delivered) volume concentration.}$$



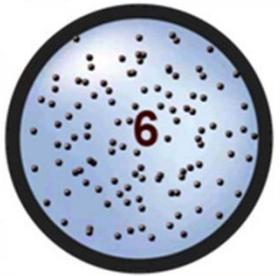
$$C_{vs} = \frac{Q_s}{Q_m} : \text{Spatial volume concentration. Generally fixed in a lab environment.}$$

Regimes with No Bed

$$C_{vs} \approx C_{vt}$$



7. Homogeneous Transport



6. Pseudo-Homogeneous Transport



5. Heterogeneous Transport



Regimes with a Sliding Bed



8. Sheet Flow

$$C_{vs} \approx C_{vt}$$

Constant C_{vs}

Constant C_{vt}



3. Sliding Bed
with
Suspension

$$C_{vs} > C_{vt}$$



4. Sliding bed
with
Suspension

$$C_{vs} > C_{vt}$$

IMPROVEMENTS

Regimes with a Fixed Bed

Constant C_{vs}

Constant C_{vt}



2. Fixed Bed with Suspension
 $C_{vs} \gg C_{vt}$



9. Fixed bed with Suspension
 $C_{vs} \gg C_{vt}$

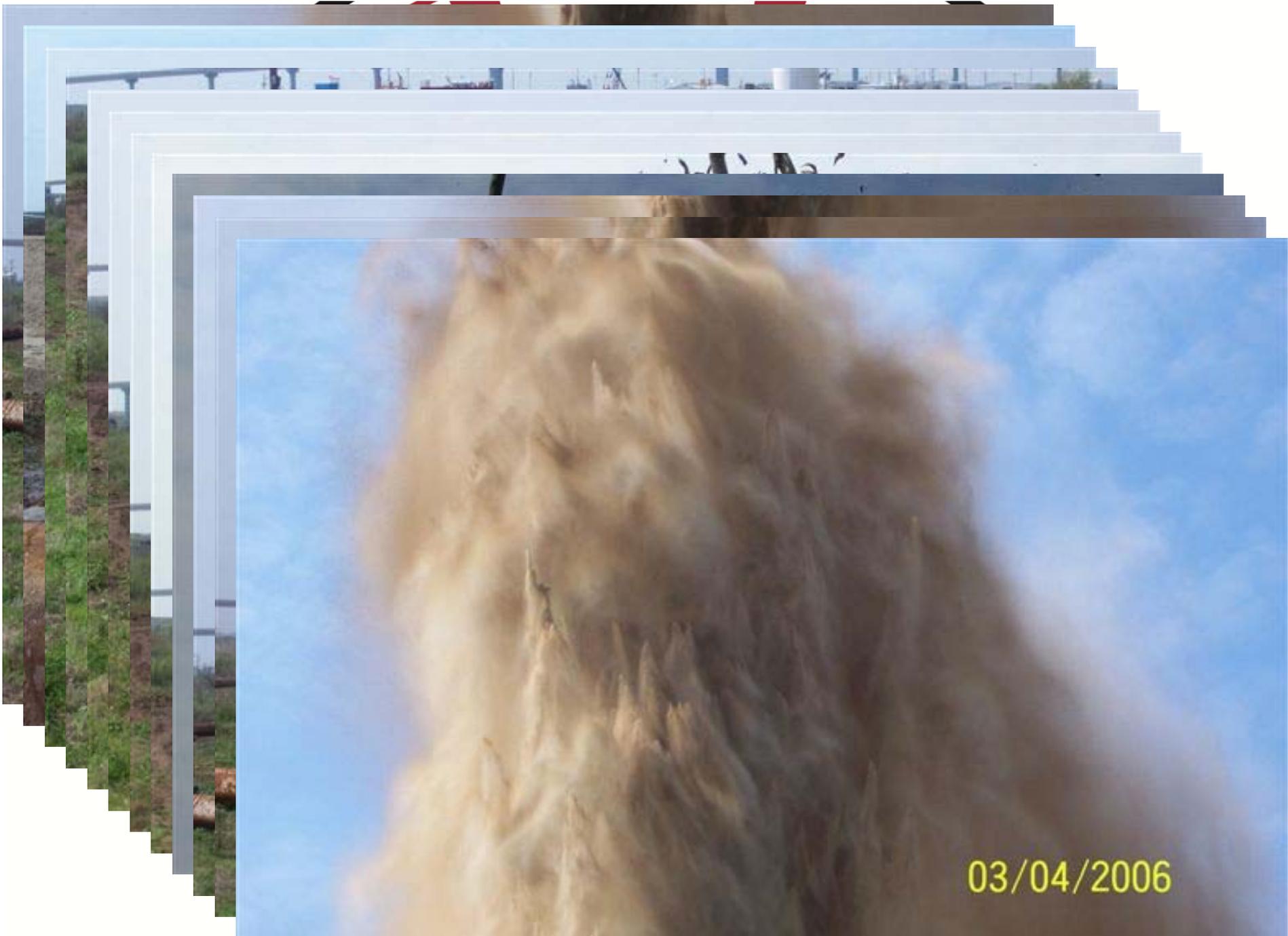


1. Fixed Bed without Suspension
Note $C_{vt} = 0!$

IMPROVEMENTS

$C_{vs} = 1.0$
 $C_{vt} = 0.0$





03/04/2006

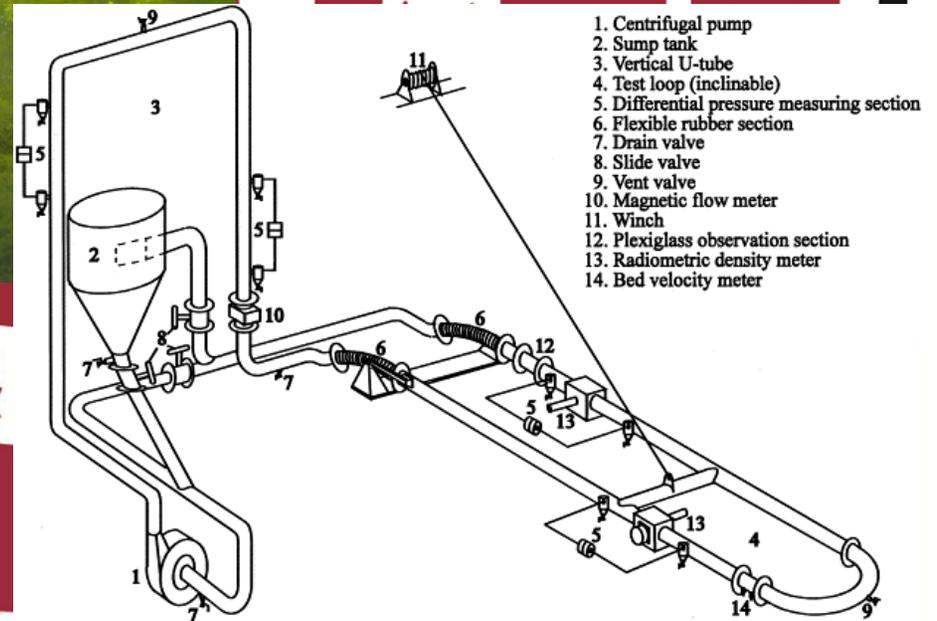
BOVEMEN

Scenarios

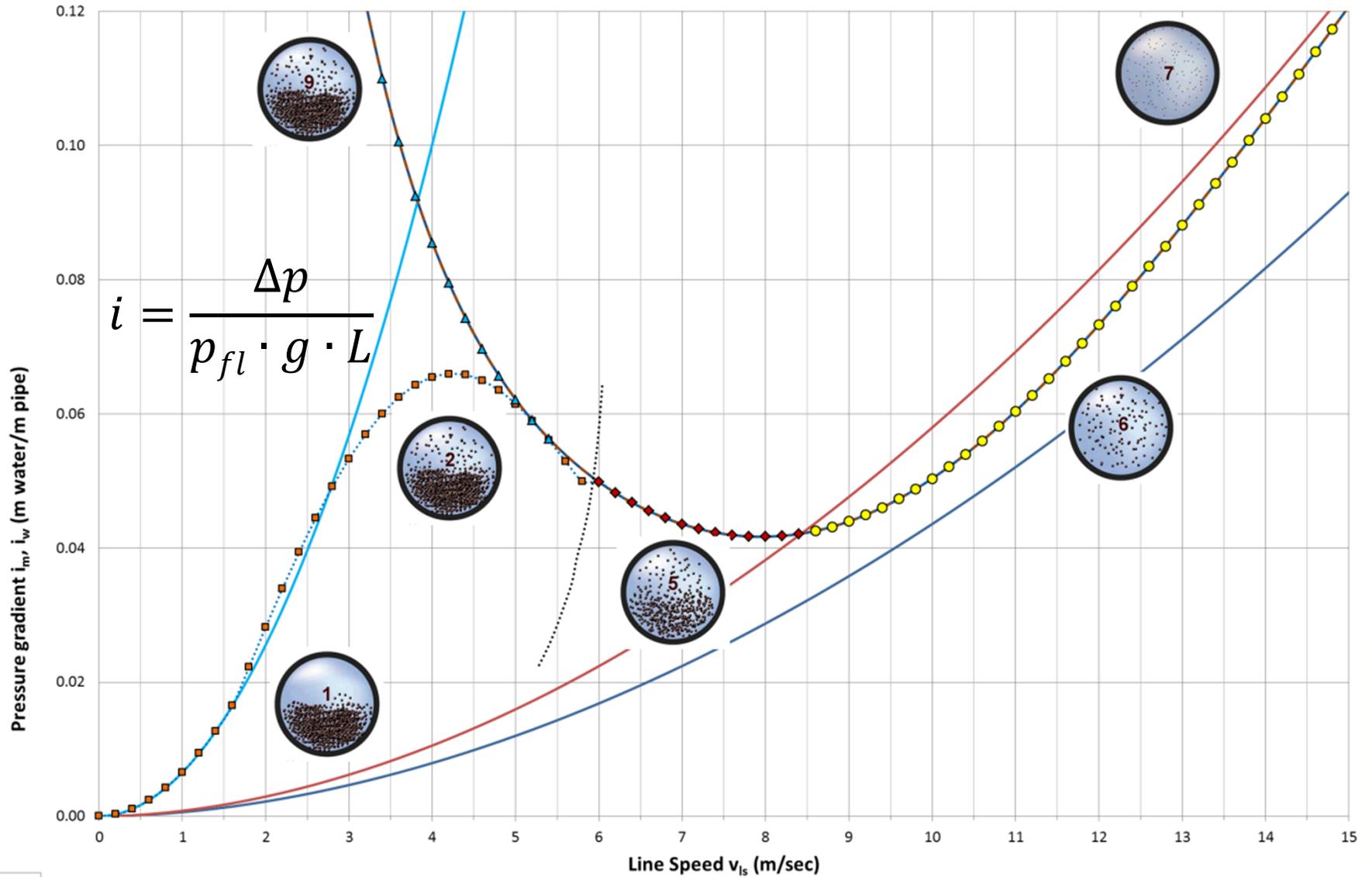


R1 – R3: Real
Life, constant
 C_{vt} (we hope)

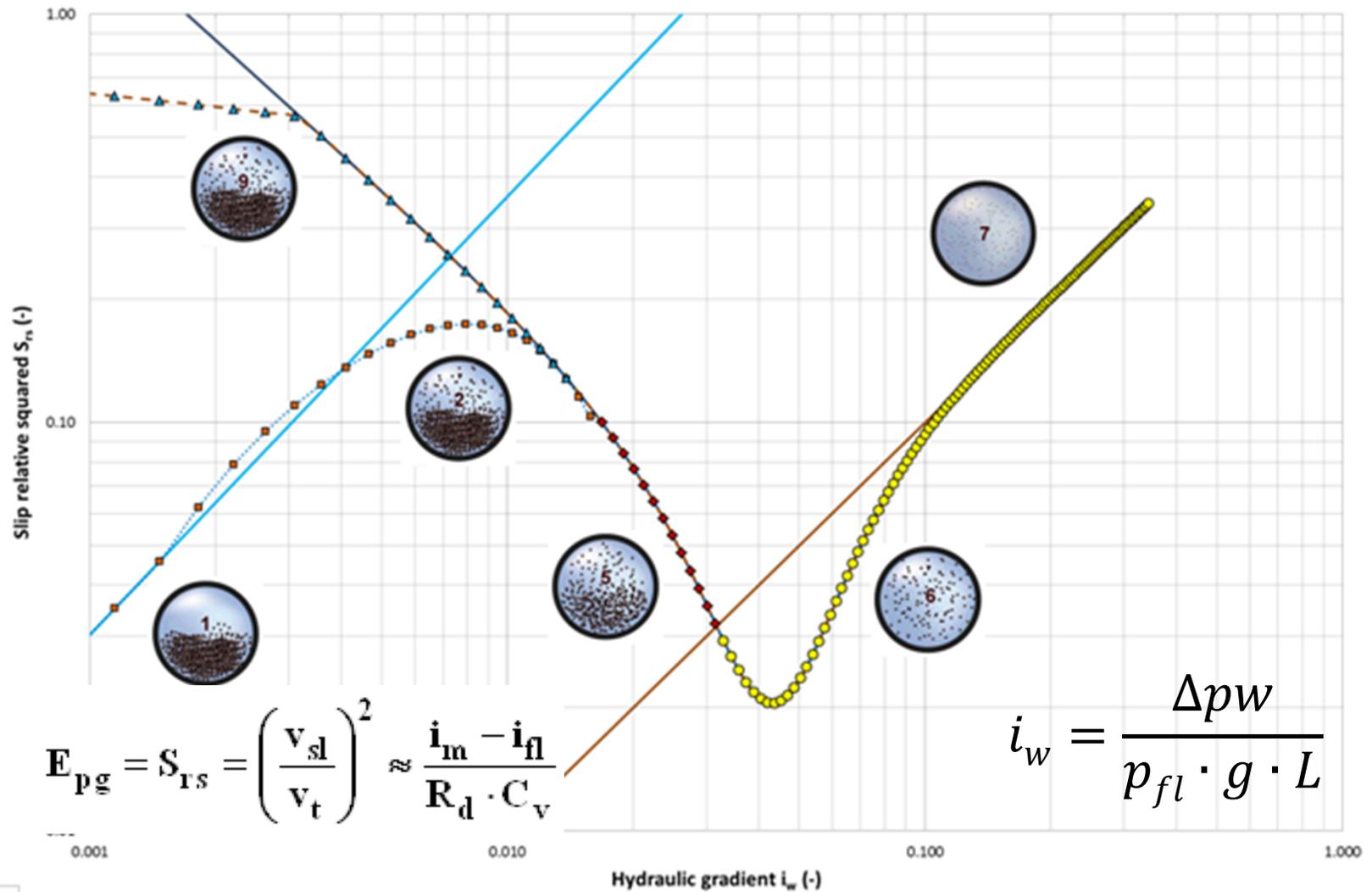
L1 – L3:
Laboratory
Setting,
constant C_{vs}



Scenario L1 & R1

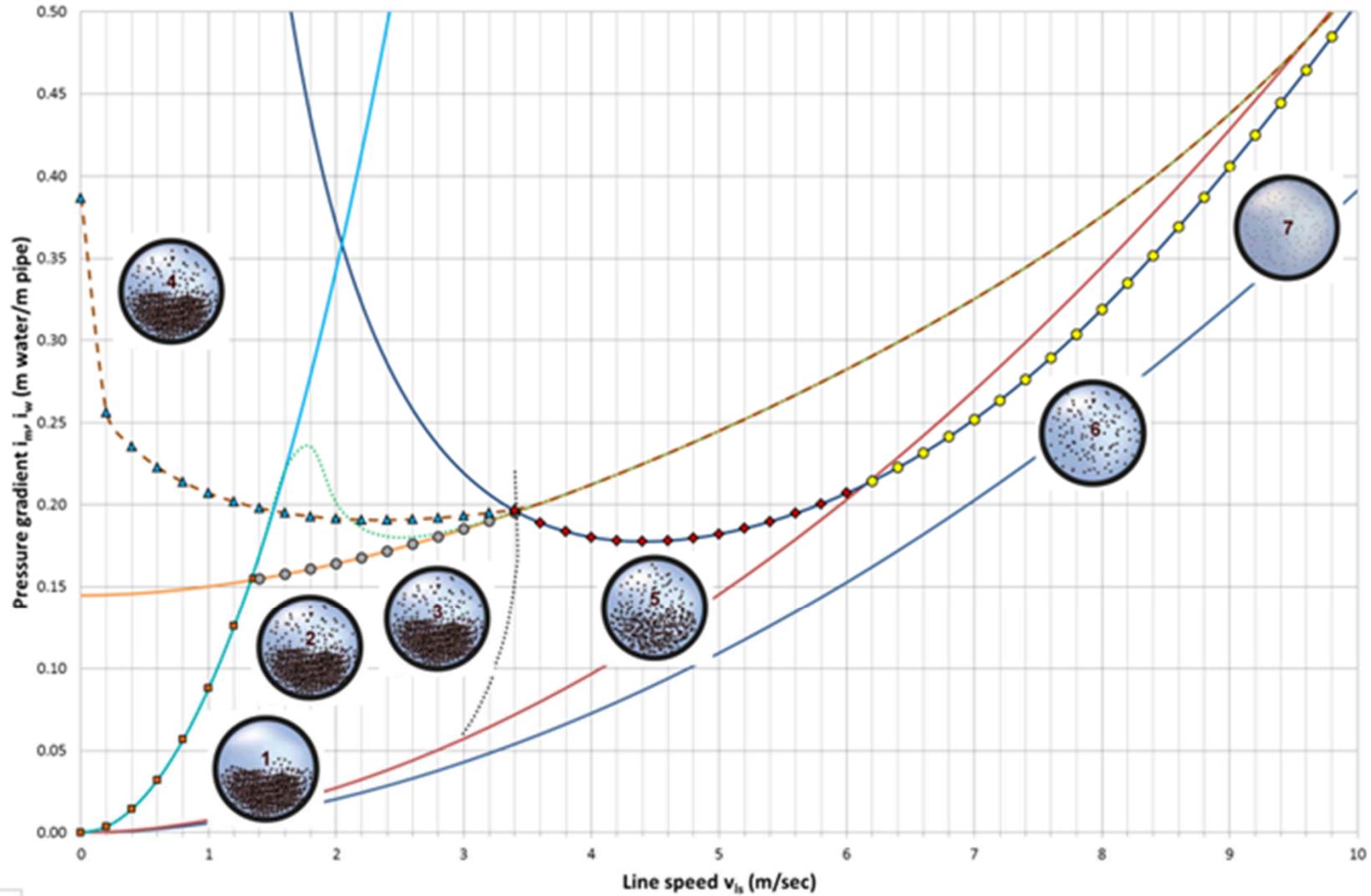


Scenario L1 & R1 (S_{rs} vs i_m)



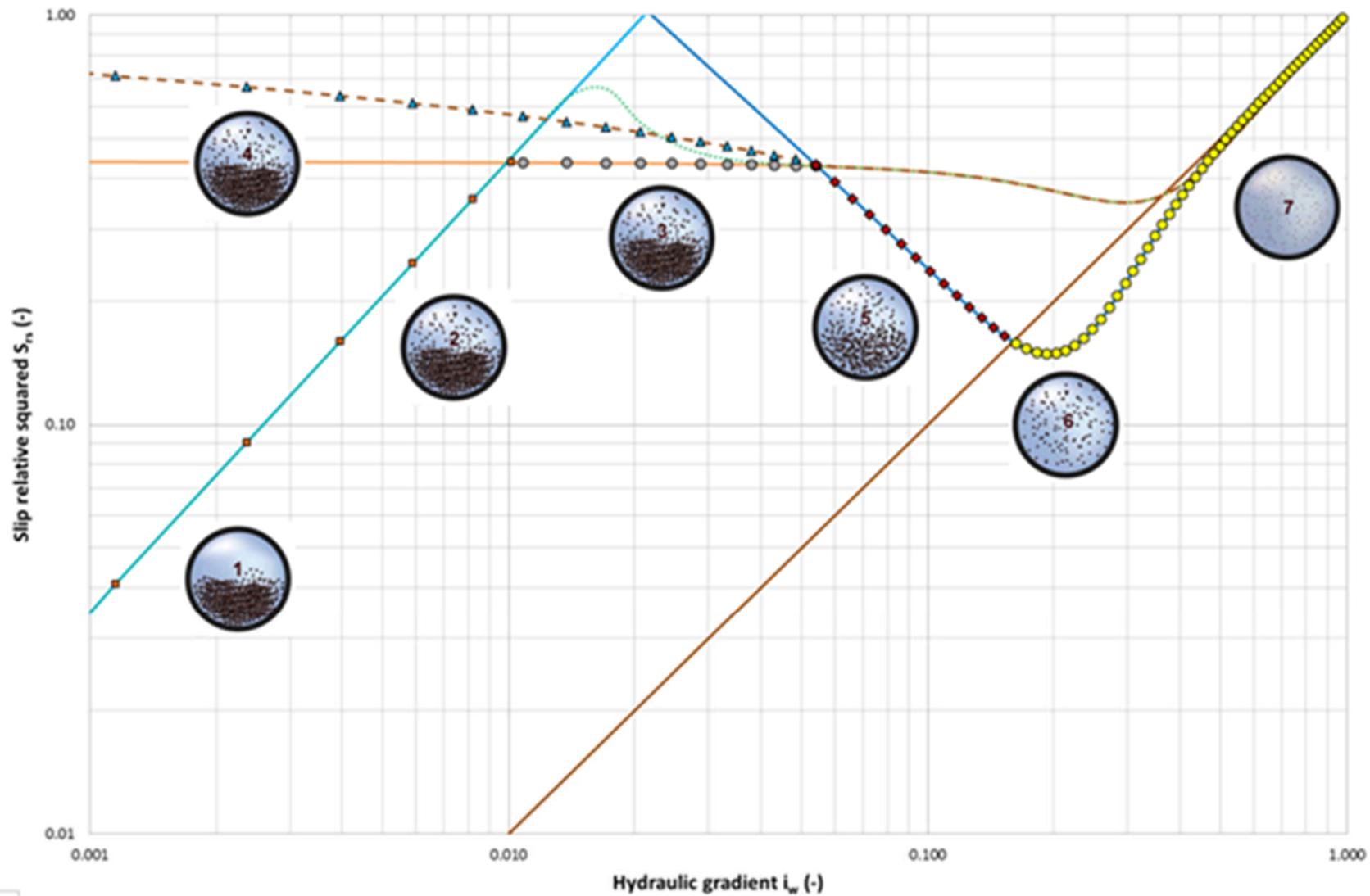
PROVEMENT

Scenario L2 & R2

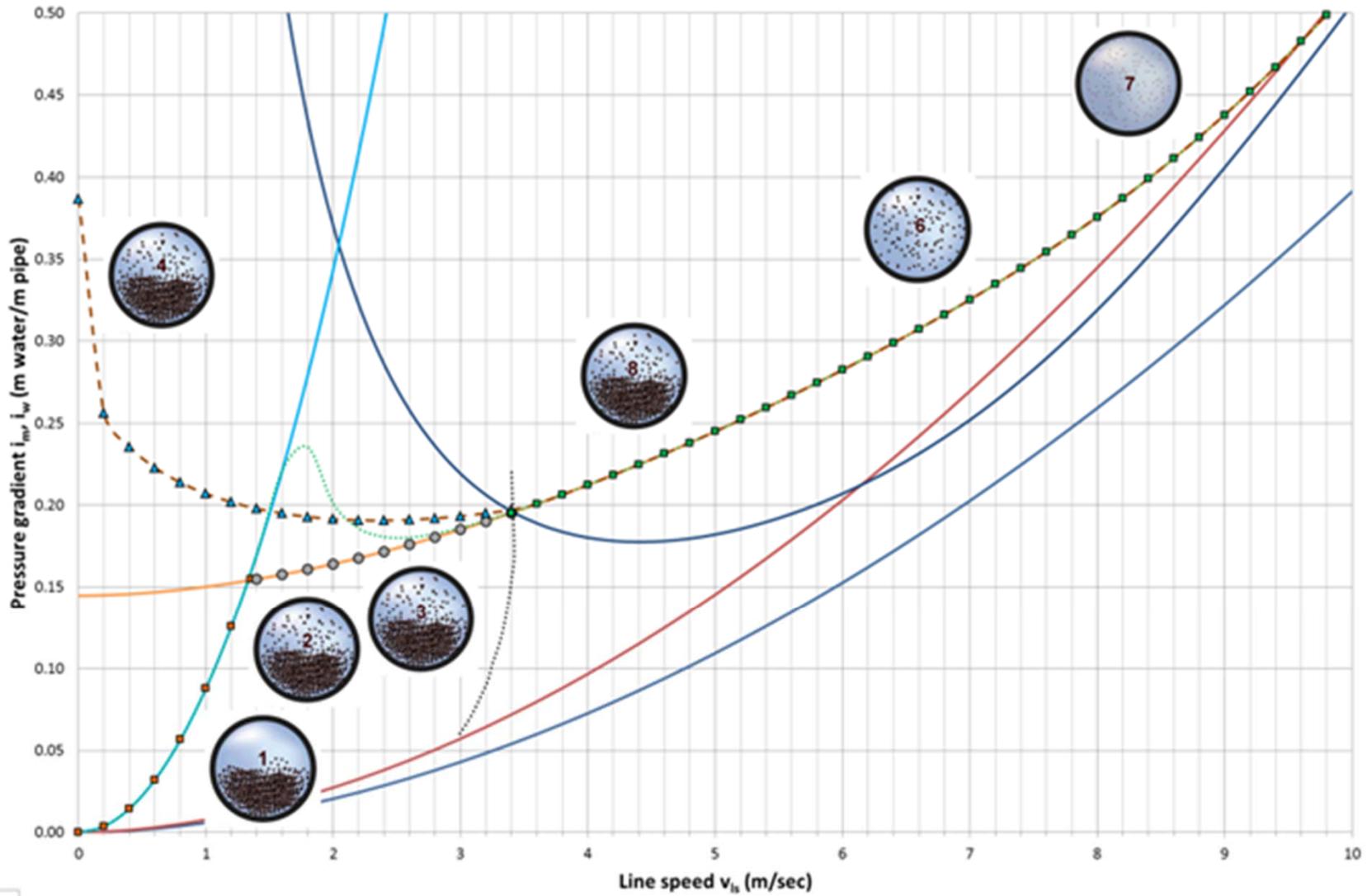


IMPROVEMENT

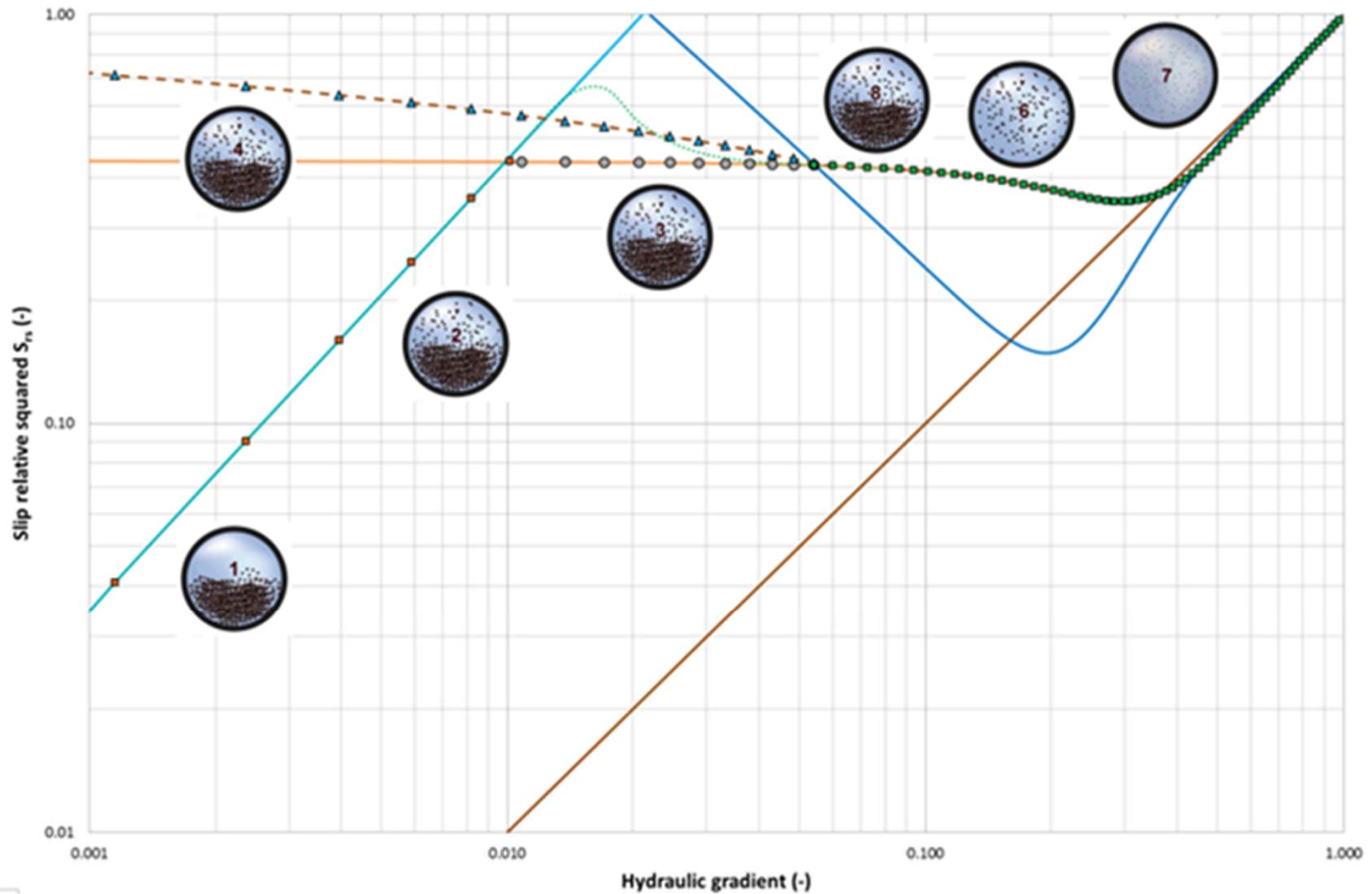
Scenario L2 & R2 (S_{rs} vs i_m)



Scenario L3 & R3



Scenario L3 & R3 (S_{rs} vs i_m)

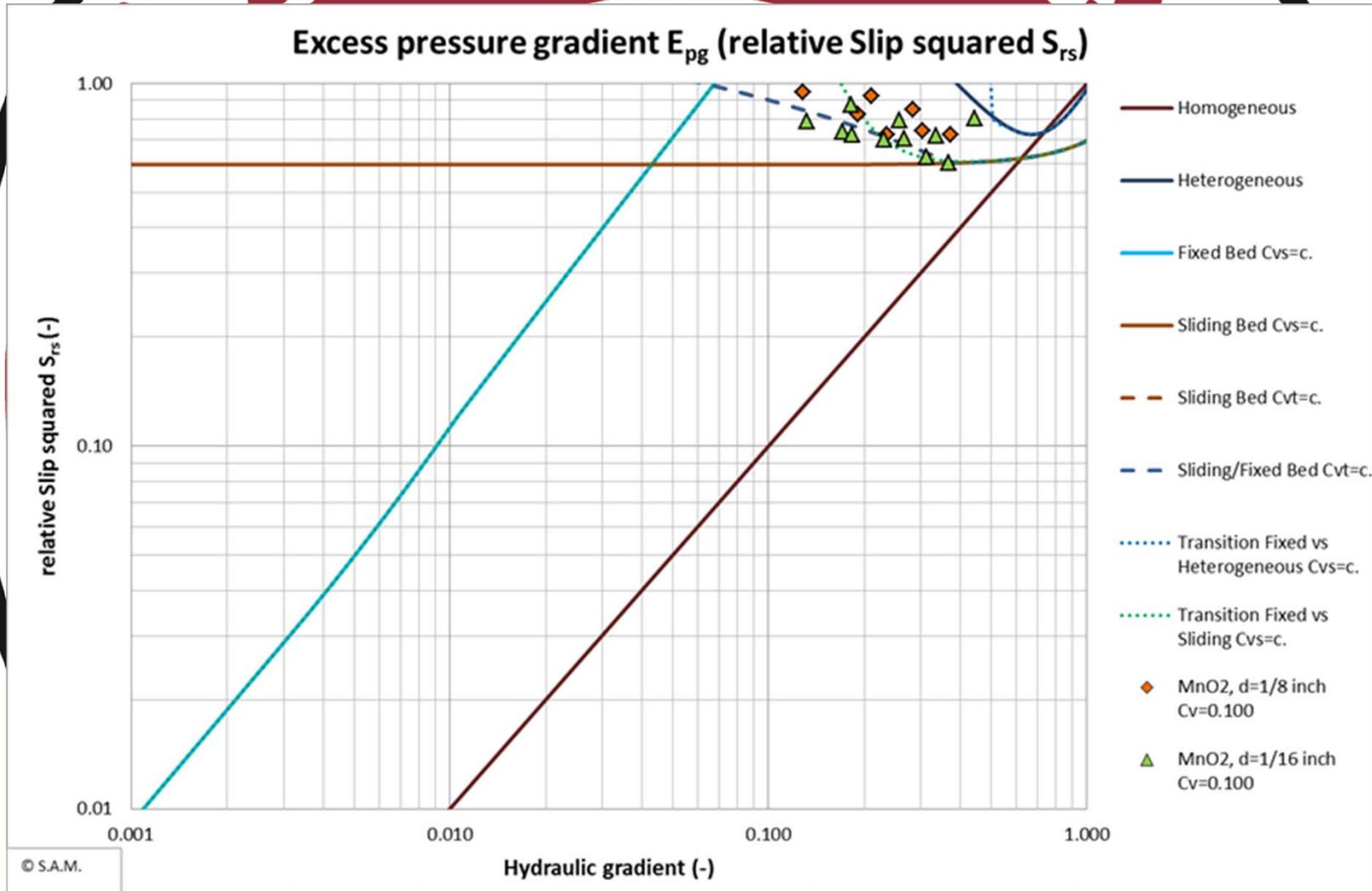


Verification/Validation



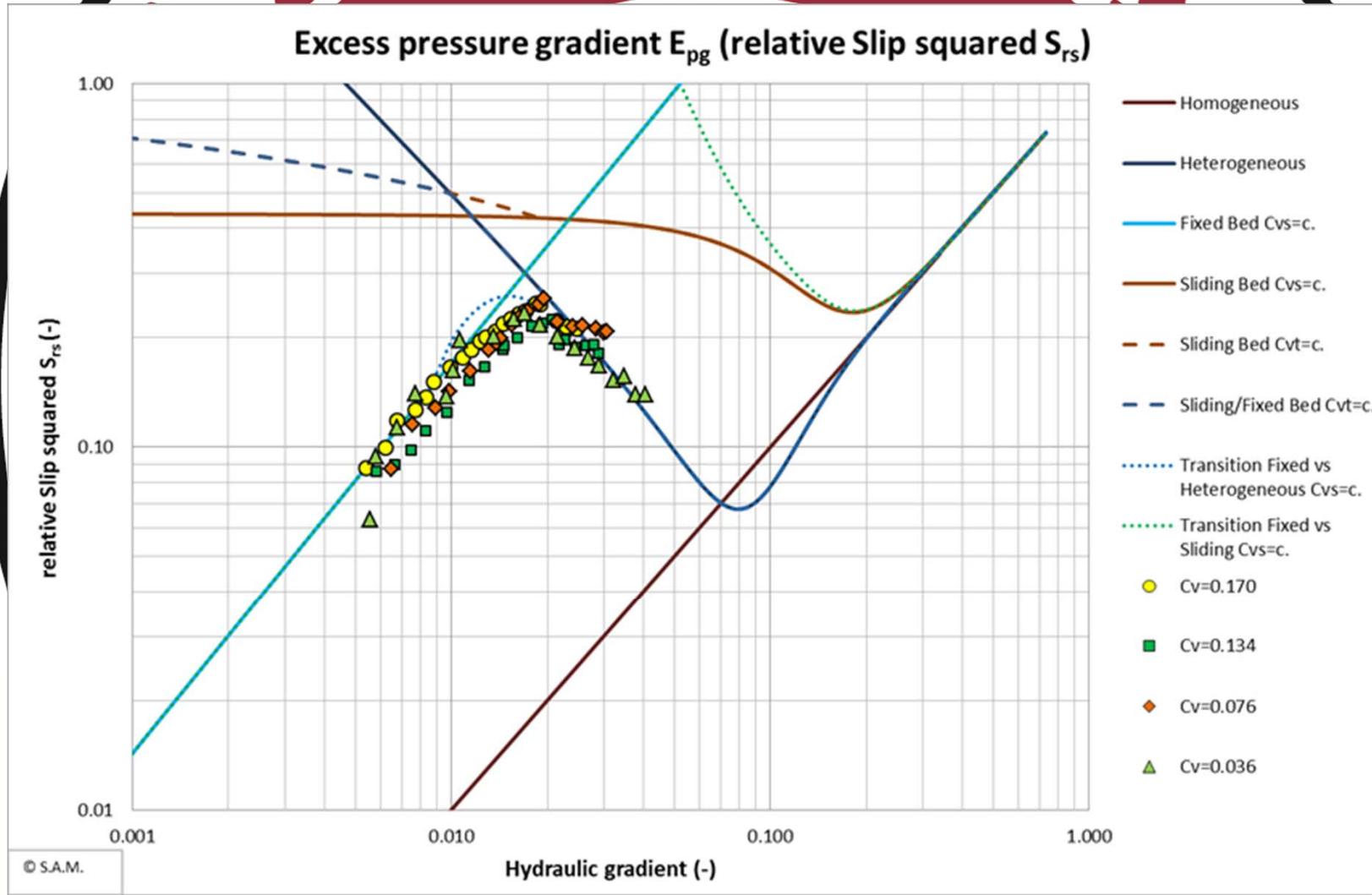
Experimental Data

Sliding Bed, $C_{vt}=c.$



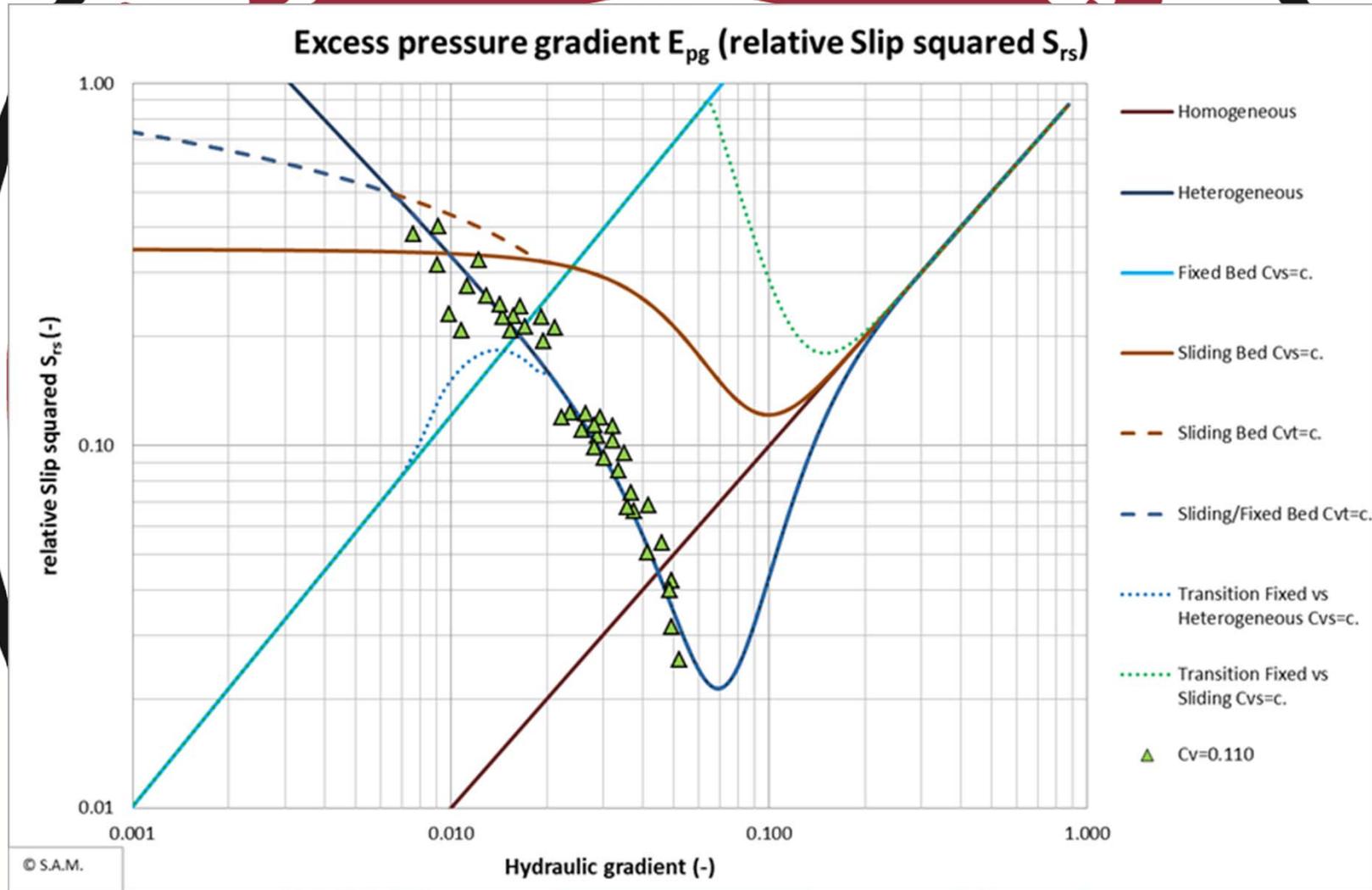
Newitt et al. (1955) $D_p = 0.025m$, $d=1.6-3.2mm$

Fixed Bed - Heterogeneous



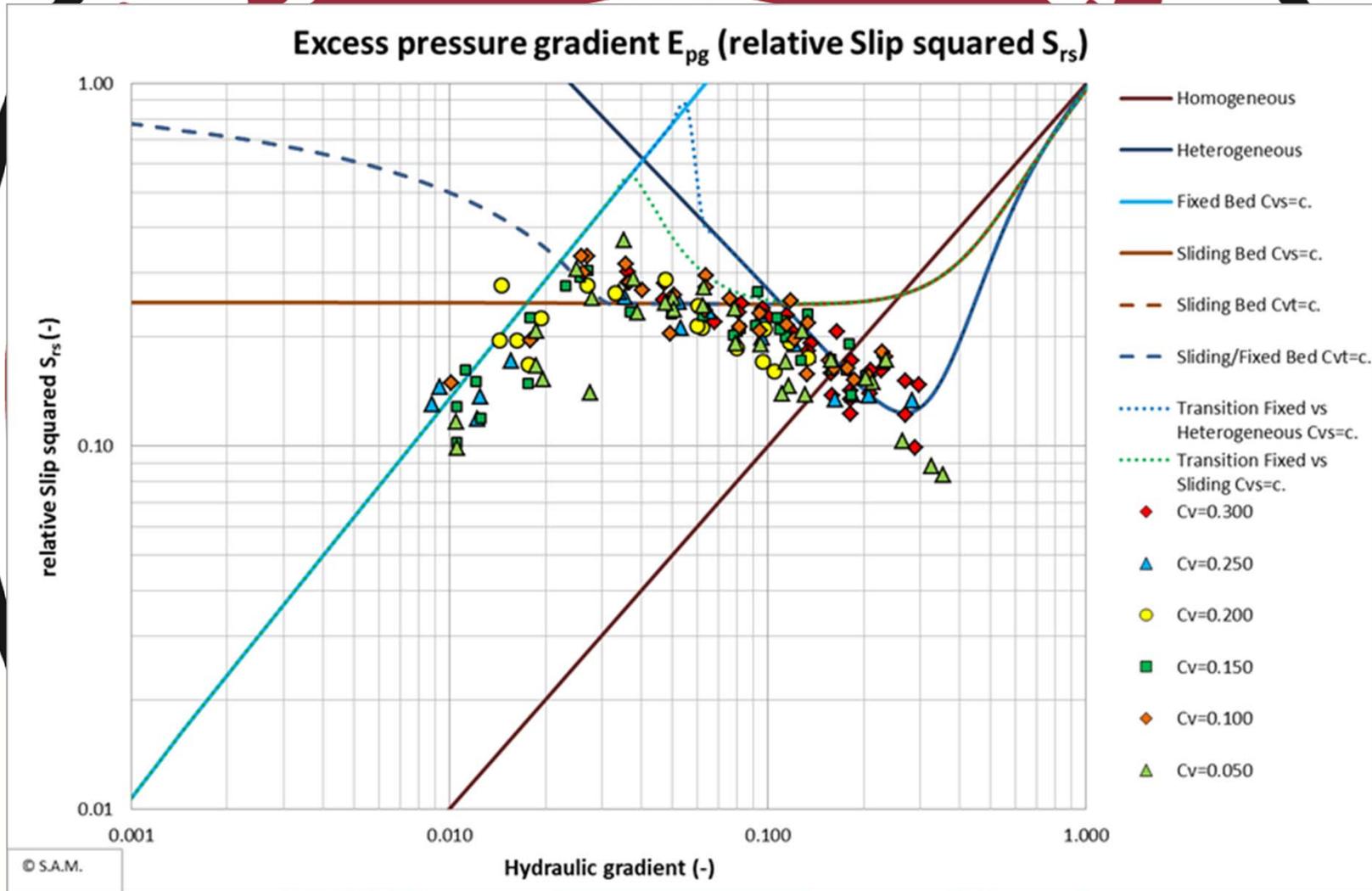
Kazanskij (1980) $D_p=0.5m$, $d=1.5mm$, C_{vs}

Heterogeneous



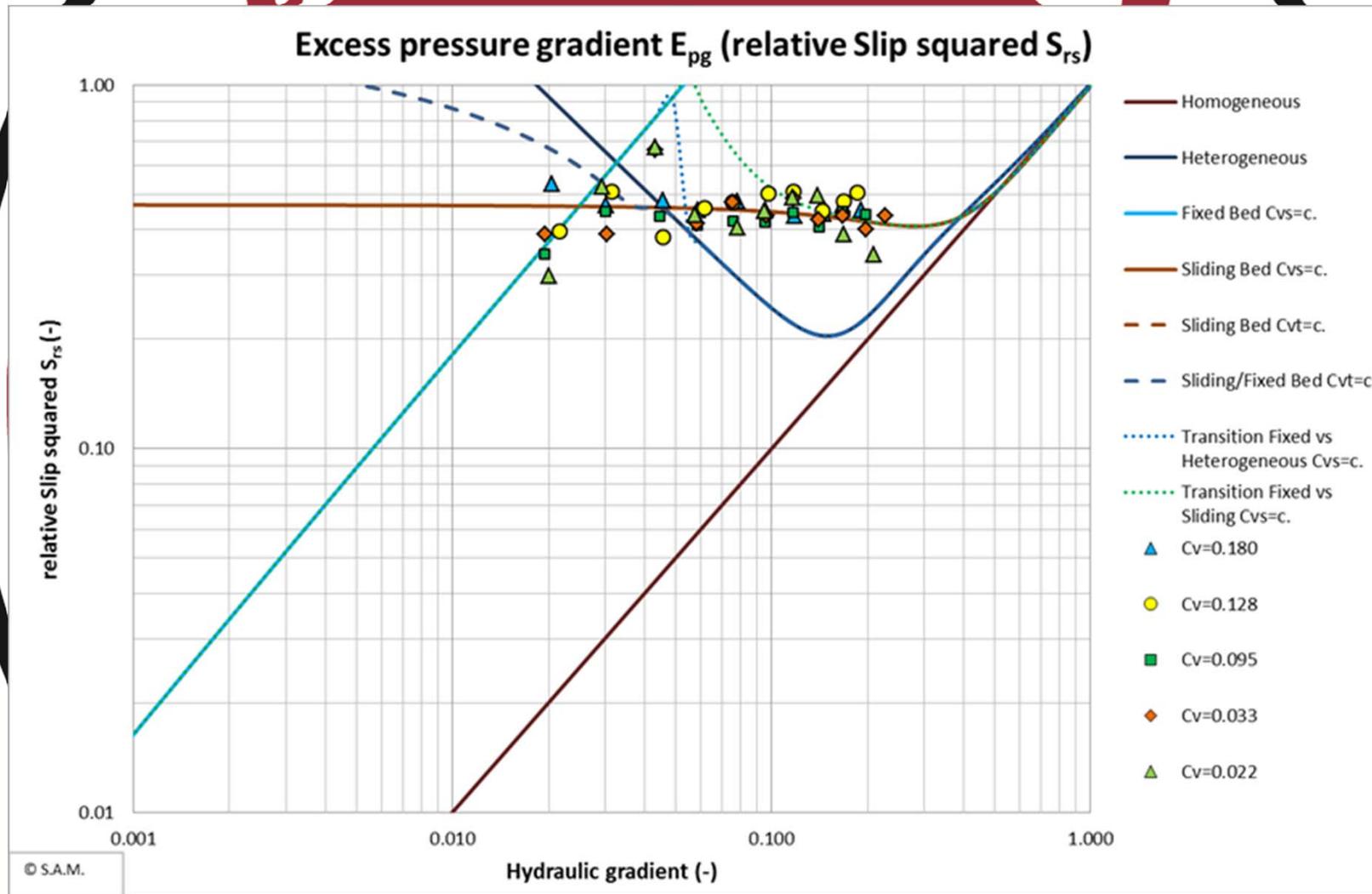
Clift et al. (1982) $D_p=0.44m$, $d=0.68mm$, C_{vt}

Fixed Bed – Sliding Bed - Heterogeneous



Wiedenroth (1967) $D_p=0.125m$, $d=2.2mm$, C_{vs}

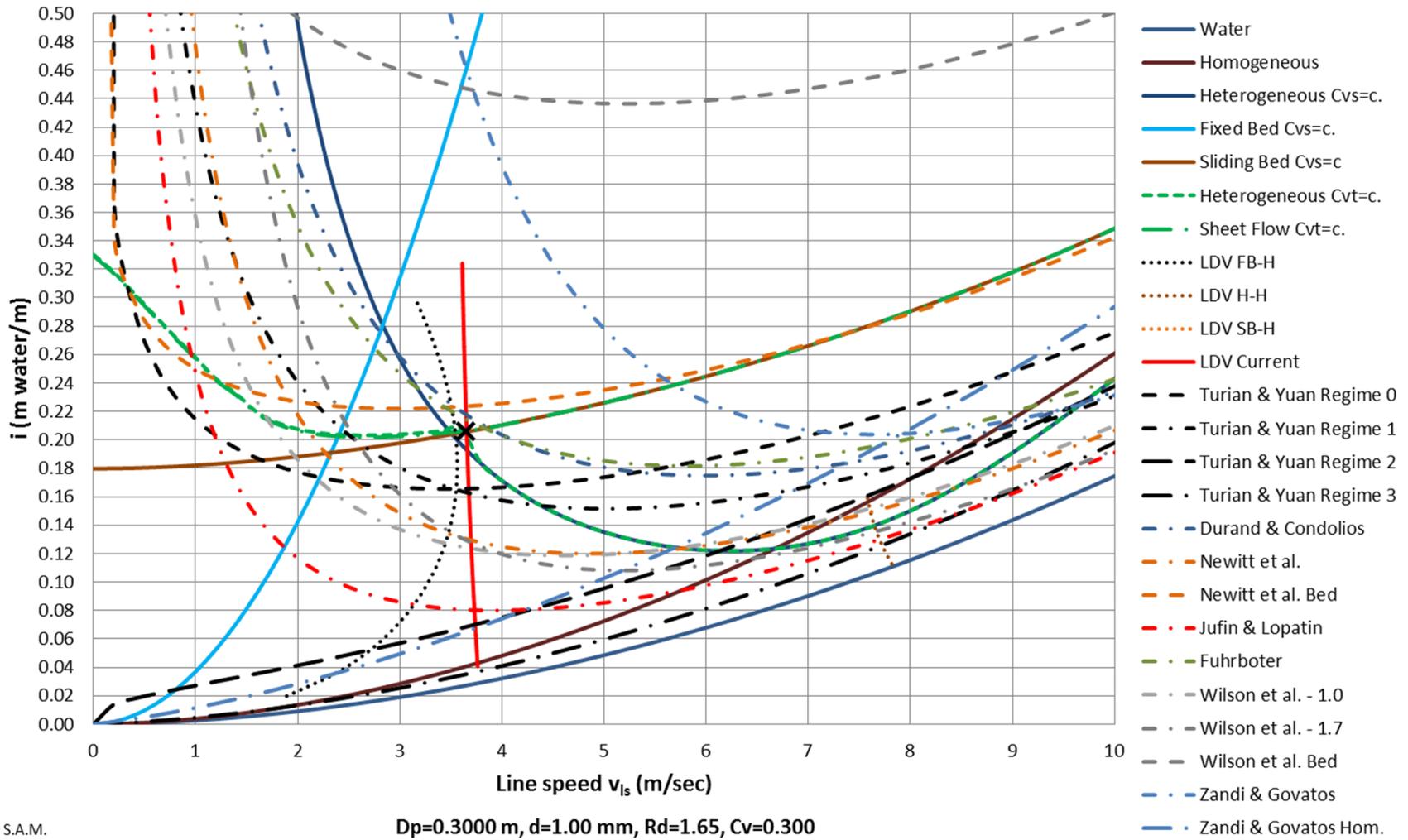
Fixed Bed – Sliding Bed - Sheet Flow



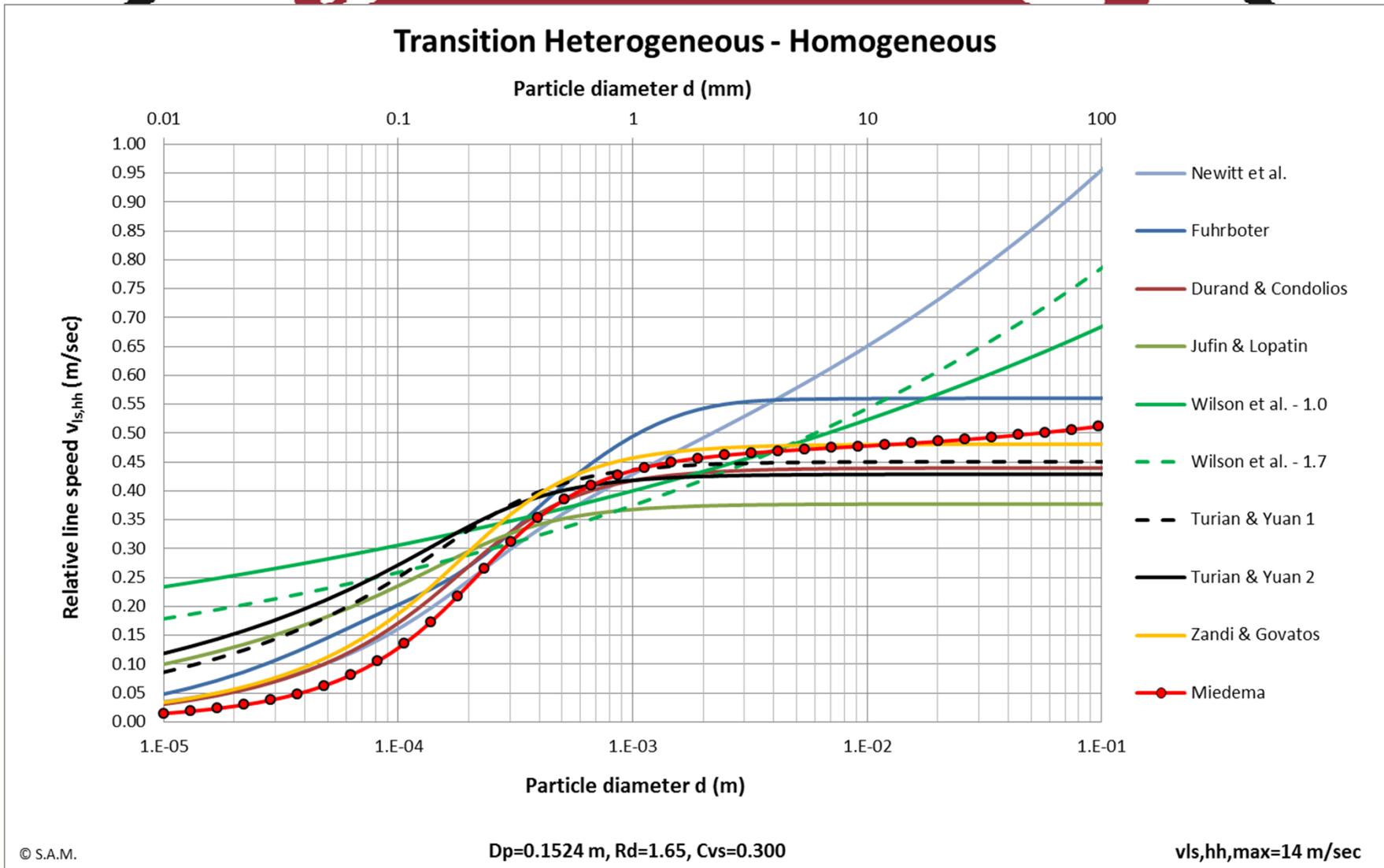
Boothroyde (1979) $D_p=0.2m$, $d=4.3mm$

21 Different Models

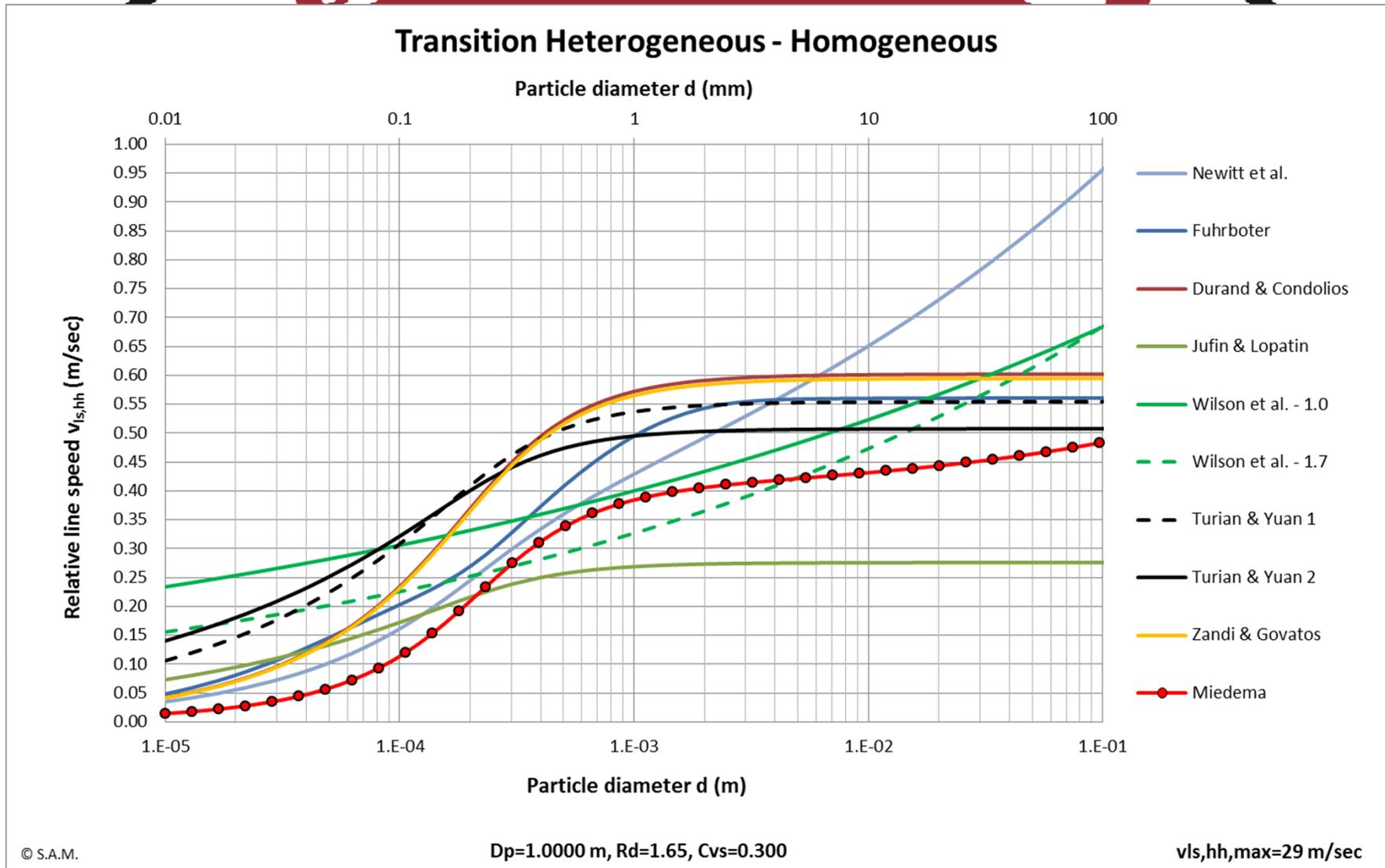
Pressure Gradient, All



Different Models for $D_p=0.15$ m, $C_v=0.30$



Different Models for $D_p=1.00$ m, $C_v=0.30$



Energy Considerations

Energy Dissipation by:

- Viscous Friction & Turbulence (Darcy Weisbach)
- Potential Energy Losses (Hindered Settling Velocity)
- Kinetic Energy Losses (Collisions)
- Sliding & Rolling Friction
- Magnus Lift Work (Viscous Sub-Layer, Low Speed)
- Turbulent Lift Work & Eddy Work (High Line Speed)

Heterogeneous Transport

- Energy Dissipation by:
- Viscous Friction & Turbulence (Darcy Weisbach)
- Potential Energy Losses (Hindered Settling Velocity)
- Kinetic Energy Losses (Collisions)

$$\Delta p_m = \Delta p_{fl,visc} + \Delta p_{s,pot} + \Delta p_{s,kin} = \Delta p_{fl,visc} \cdot \left(1 + \frac{\Delta p_{s,pot}}{\Delta p_{fl,visc}} + \frac{\Delta p_{s,kin}}{\Delta p_{fl,visc}} \right)$$

Details:

Sape A. Miedema, Robert C. Ramsdell (2013):

A HEAD LOSS MODEL FOR SLURRY TRANSPORT BASED ON ENERGY CONSIDERATIONS

WODCON XX. Brussels, Belgium.: WODA

Conclusions – Regimes and Results

- 9 Flow regimes can be distinguished. Not every flow regime is present for every combination of particles, pipe and concentration.
- It is crucial to distinguish between constant volumetric spatial and transport concentration in interpreting experimental results.
- With a good model for each flow regime, the scenarios can be constructed and the correct flow regime can be predicted.



Questions?