



# Cutter Head Spillage

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# Dredging A Way Of Life



# Offshore A Way Of Life



# What is Offshore & Dredging Engineering?

Offshore & Dredging Engineering covers everything at sea that does not have the purpose of transporting goods & people and no fishery.





# The Cutter Head

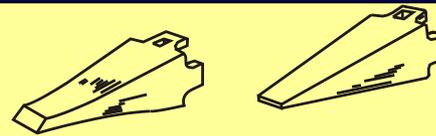
# The Mashour



# Rock Cutter Heads



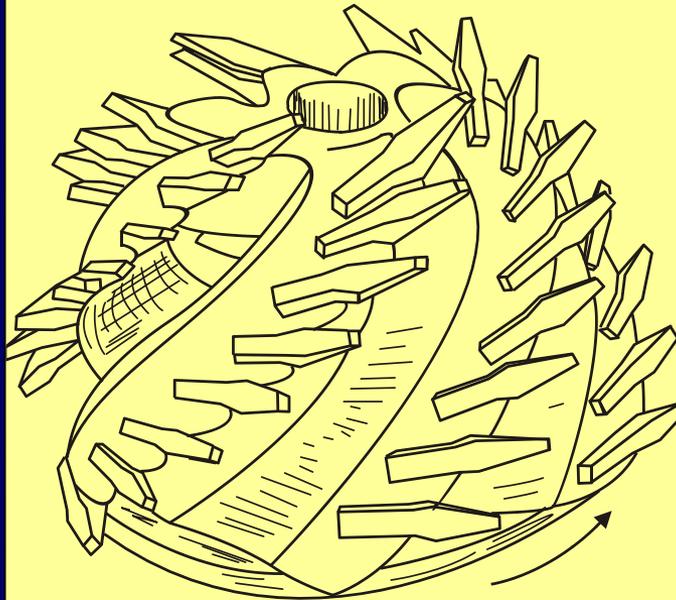
"PICK-POINT"



NARROW CHISELS



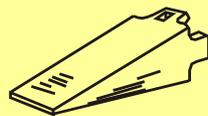
TRAPEZOIDALE PICK-POINT



NORMAL HELIX CUTTER



REVERSE HELIX CUTTER



WIDE CHISEL



CL FLARED



BELOW CL FLARED

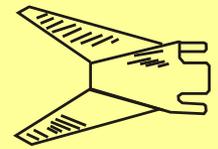
TYPE A

breaking-edge



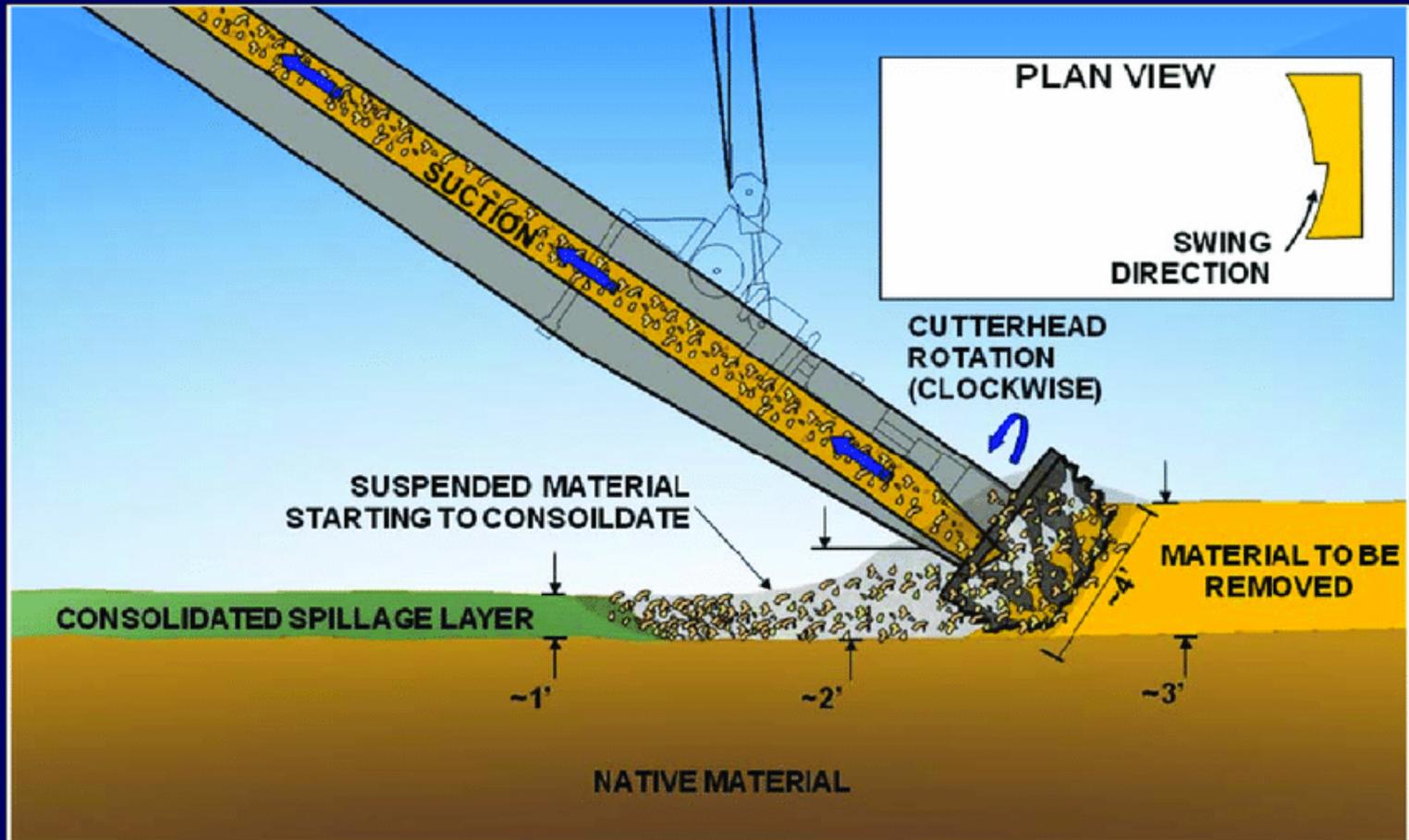
BELOW CL FLARED

TYPE B (CLAY FLARE)

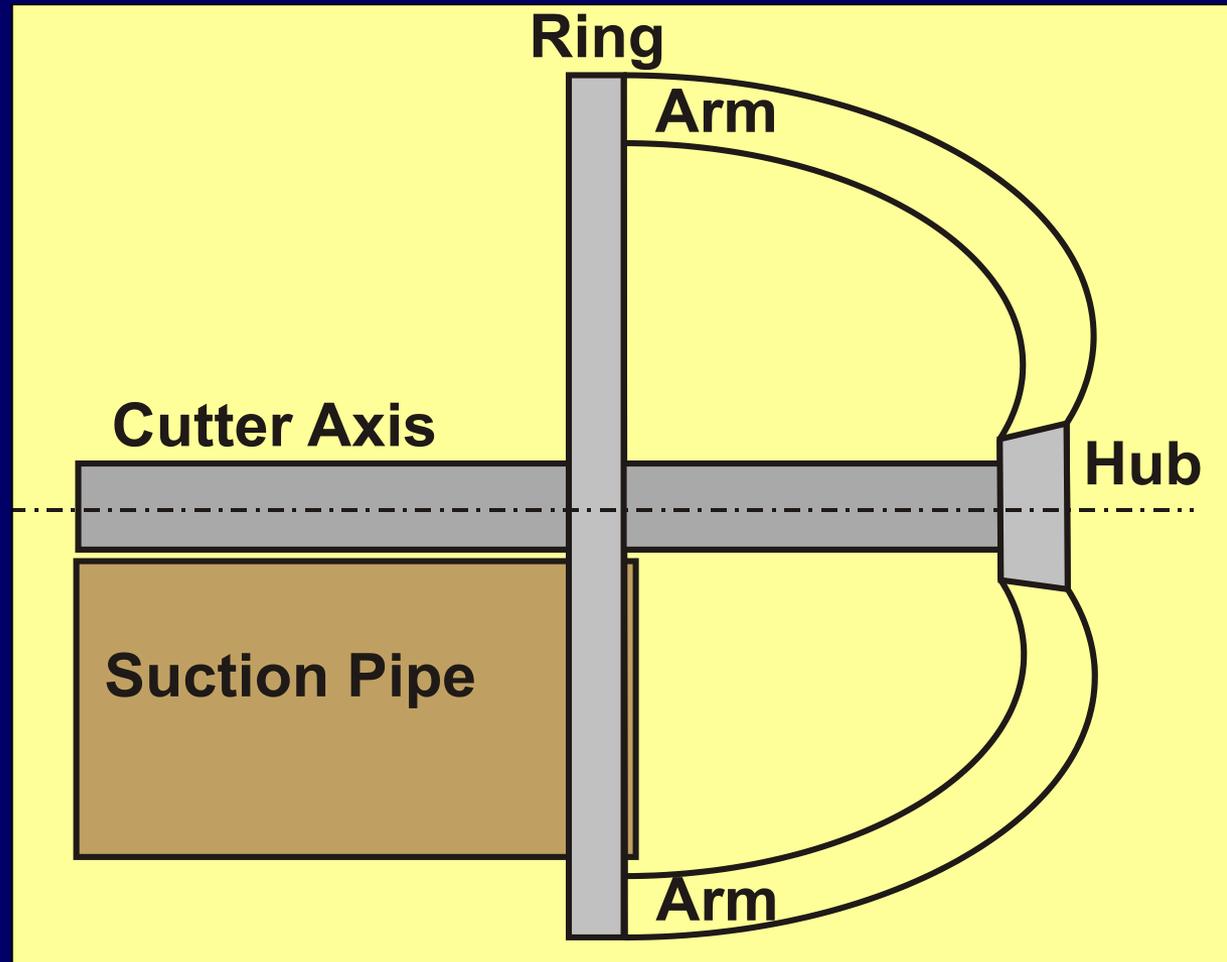


"DEVIL TEETH"  
(FLORIDA)

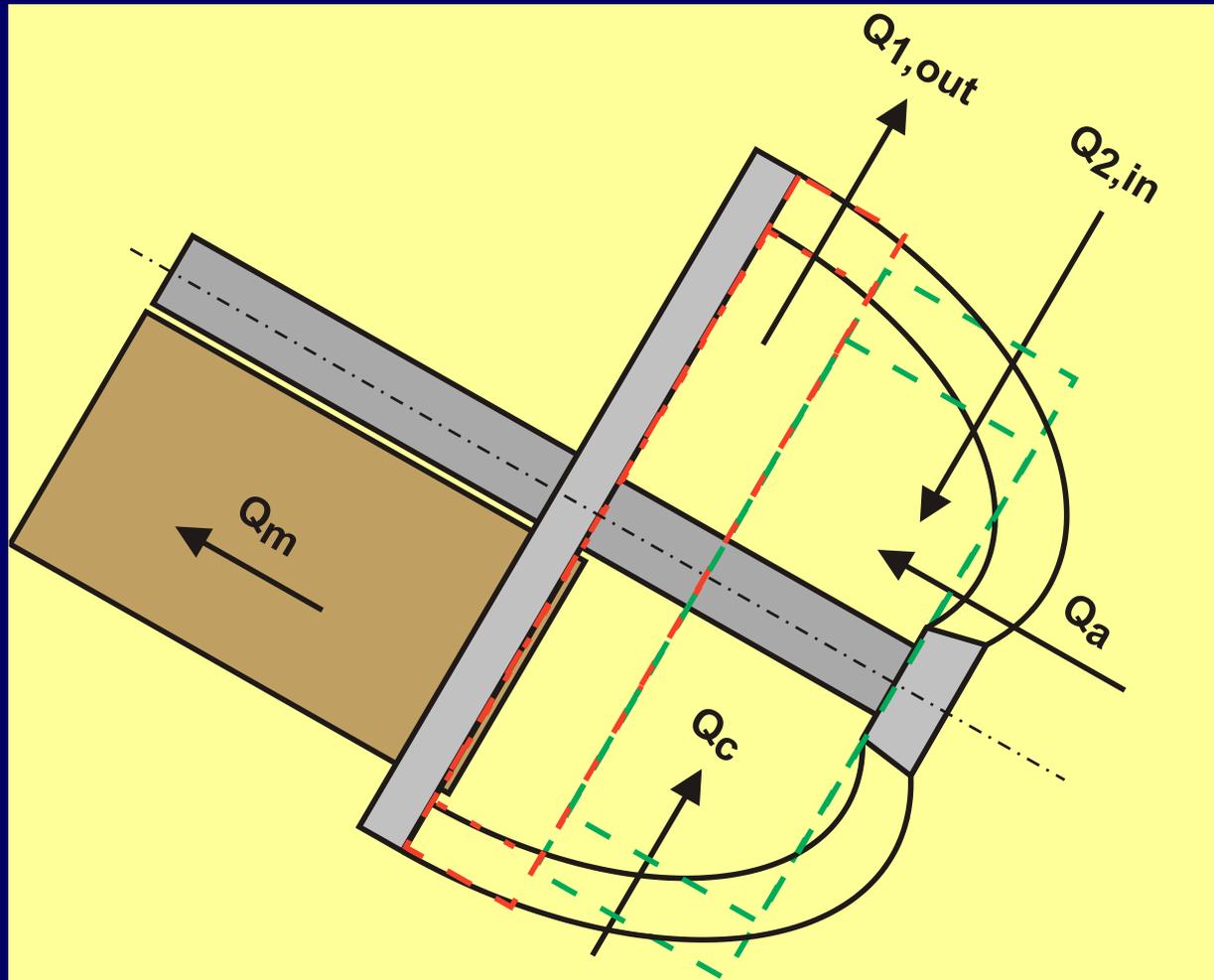
# Spillage



# Definitions



# Different Flows in a Drag Head





# Affinity Law Model

# Affinity Laws

$$F = m \cdot \omega^2 \cdot R \quad \text{with: } m = \rho_m \cdot \frac{\pi}{4} \cdot D^2 \cdot w$$

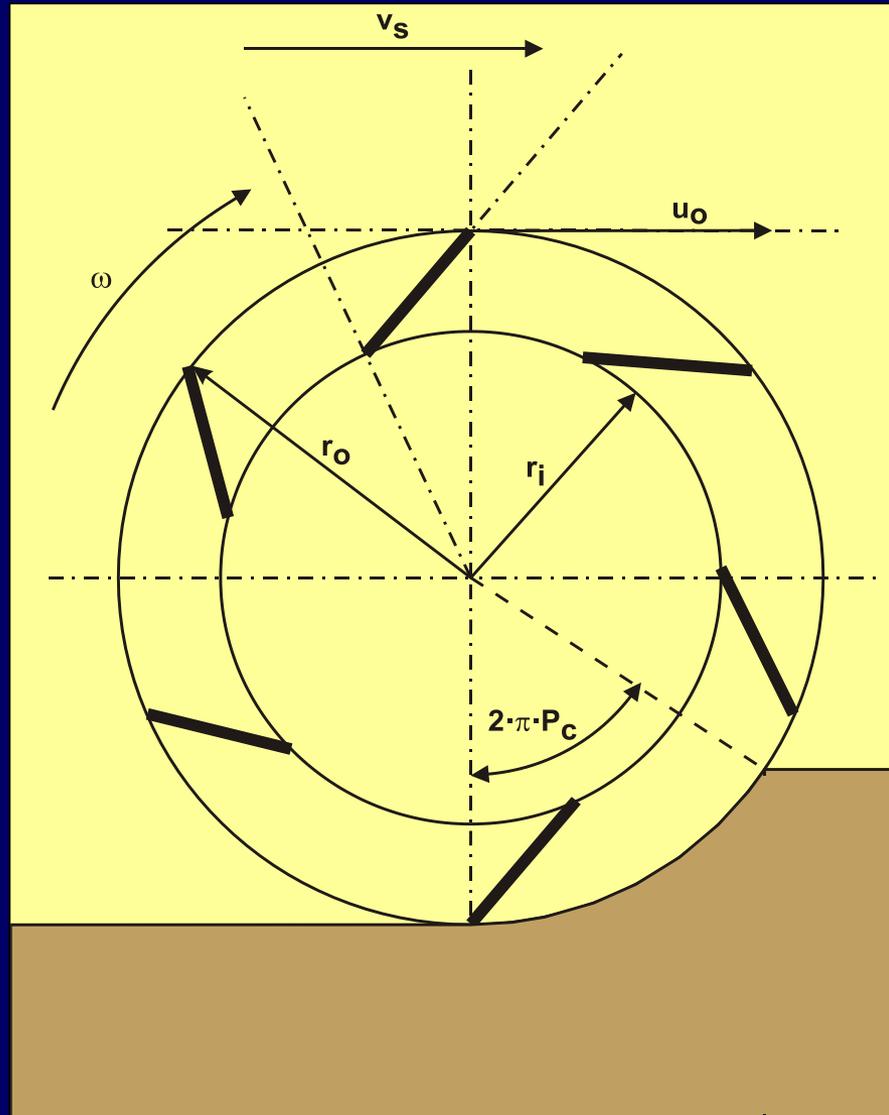
$$p = \frac{F}{A} = \frac{\rho_m \cdot \frac{\pi}{4} \cdot D^2 \cdot w \cdot \omega^2 \cdot R}{\pi \cdot D \cdot w} = \frac{1}{8} \cdot \rho_m \cdot \omega^2 \cdot D^2$$

$$Q = \omega \cdot R \cdot \pi \cdot D \cdot w = \frac{\pi}{2} \cdot \omega \cdot D^2 \cdot w$$

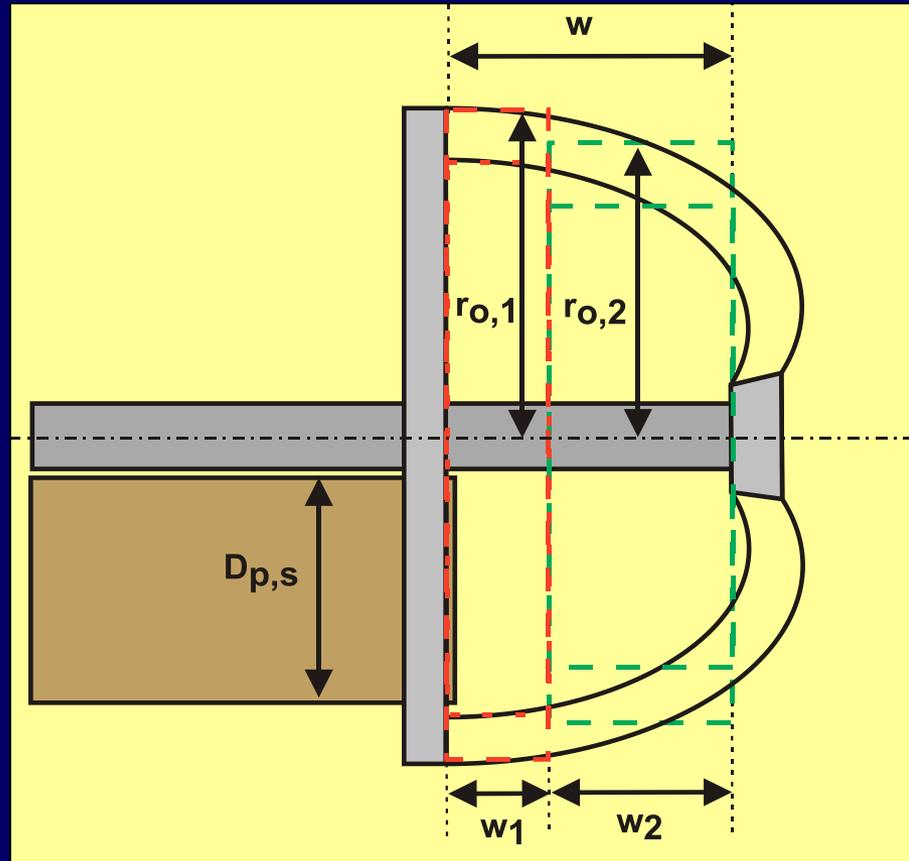
$$\frac{\eta_1}{\eta_2} = 1 \quad \text{and} \quad \frac{p_1}{p_2} = \frac{n_1^2}{n_2^2} \cdot \frac{D_1^2}{D_2^2} \cdot \frac{\rho_{m1}}{\rho_{m2}} \quad \text{and} \quad \frac{Q_1}{Q_2} = \frac{n_1}{n_2} \cdot \frac{D_1^2}{D_2^2} \cdot \frac{w_1}{w_2}$$

$$\frac{P_1}{P_2} = \frac{n_1^3}{n_2^3} \cdot \frac{D_1^4}{D_2^4} \cdot \frac{\rho_{m1}}{\rho_{m2}} \cdot \frac{w_1}{w_2} \quad \text{and} \quad \frac{T_1}{T_2} = \frac{n_1^2}{n_2^2} \cdot \frac{D_1^4}{D_2^4} \cdot \frac{\rho_{m1}}{\rho_{m2}} \cdot \frac{w_1}{w_2}$$

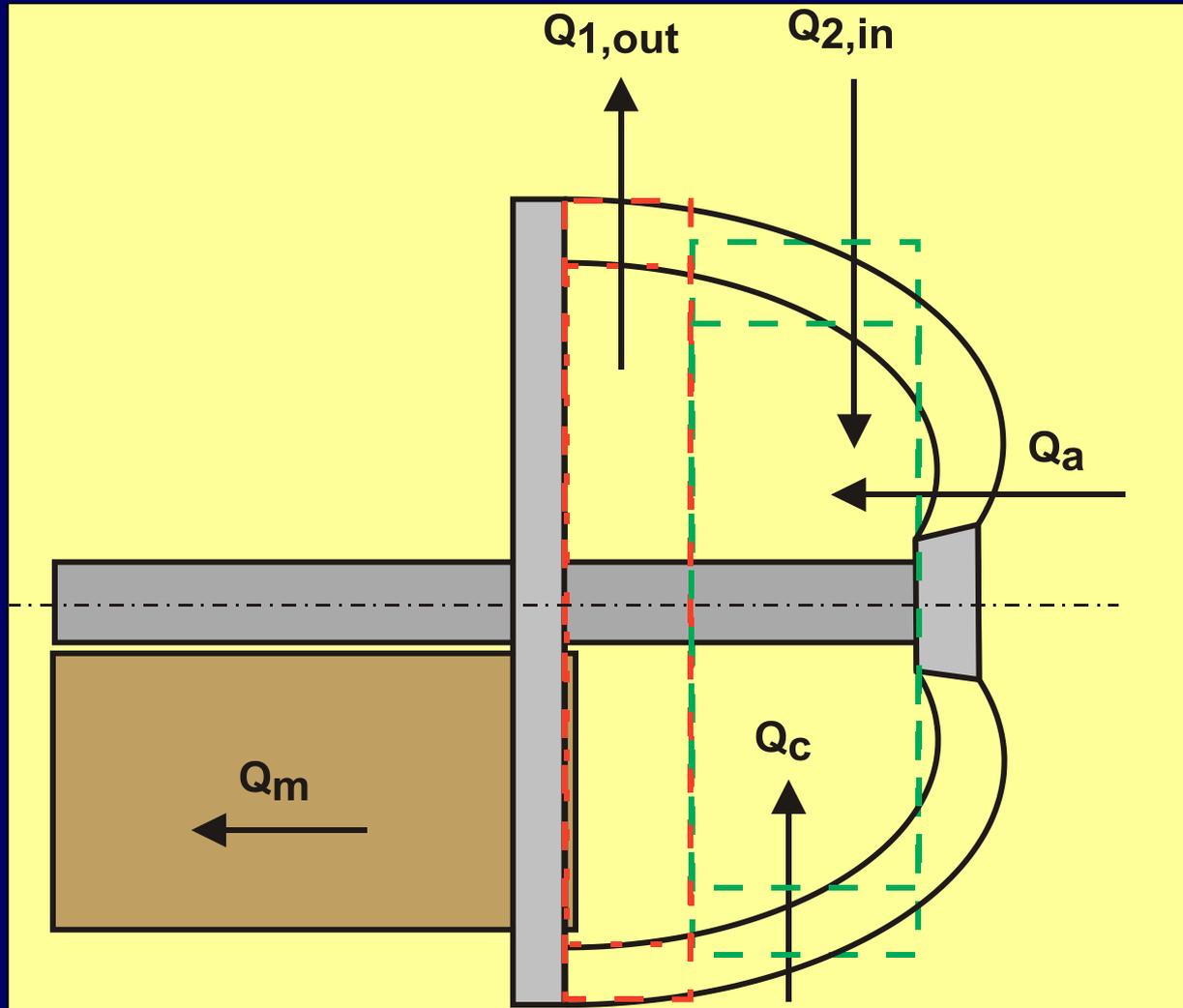
# Cutter Head Dimensions



# Cutter Head Segments



# The Flows in a Cutter Head



# Flows & Spillage Homogeneous

$$Q_{1,out} = \alpha \cdot 2 \cdot \pi \cdot \omega \cdot r_{o,1}^2 \cdot$$

$$\left( \frac{f}{(1+f)} \cdot w - \frac{1}{(1+f)} \cdot \frac{1}{2 \cdot \pi \cdot \alpha \cdot \omega} \cdot \left( \frac{Q_m - Q_c - Q_a}{r_{o,1}^2 \cdot (1 - P_c)} \right) \right) \cdot (1 - P_c)$$

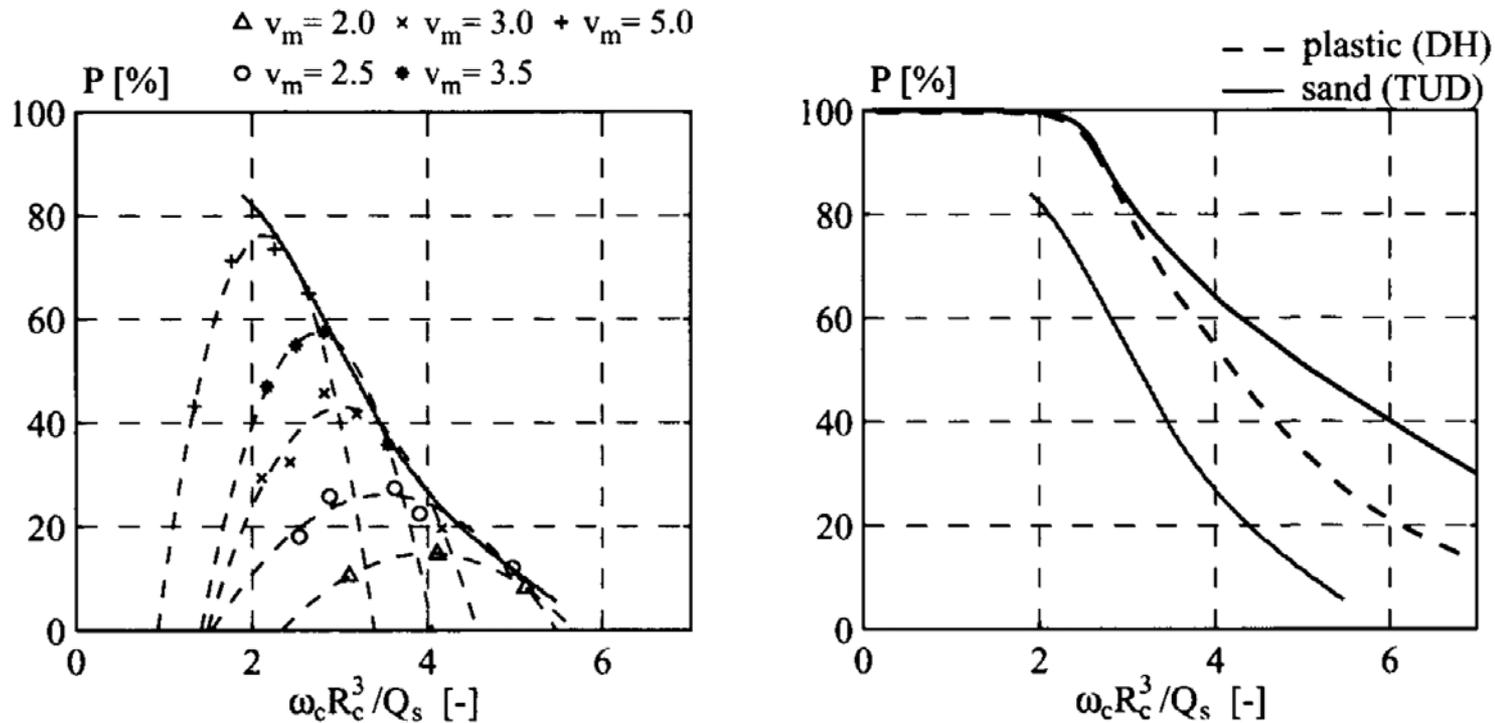
$$Q_{2,in} = 2 \cdot \pi \cdot \alpha \cdot \omega \cdot (r_{o,1}^2 - r_{o,2}^2) \cdot$$

$$\left( \frac{1}{(1+f)} \cdot w + \frac{1}{(1+f)} \cdot \frac{1}{2 \cdot \pi \cdot \alpha \cdot \omega} \cdot \left( \frac{Q_m - Q_c - Q_a}{r_{o,1}^2 \cdot (1 - P_c)} \right) \right) \cdot (1 - P_c)$$

$$\text{Spillage} = \frac{Q_{1,out}}{Q_m + Q_{1,out}} = \frac{Q_{1,out} \cdot C_{vs}}{Q_s}$$

$$C_{vs} = \frac{Q_s}{Q_m + Q_{1,out}}$$

# Production den Burger



**Figure 6.7:** Production percentage vs. inverse of the flow number in the under-cut situation for cutting of gravel (left plot) and the results of the sand and plastic particles (right plot)

# Scale Laws

$$\frac{Q_c \cdot (1-n)}{Q_m} = \text{constant}$$

$$Bu = \frac{\omega \cdot r_r^3}{Q_m} = \text{constant}$$

$$\frac{v_t \cdot r_r^2}{Q_m} = \text{constant}$$

$$\frac{\omega \cdot r_r}{v_t} = \text{constant}$$



# Spillage Non-Homogeneous

$$\text{Spillage} = \frac{Q_{1,\text{out}}}{Q_m + Q_{1,\text{out}}} = \frac{Q_{1,\text{out}} \cdot C_{\text{vs}}}{Q_s}$$

$$\text{Spillage} = \frac{Q_{1,\text{out}} \cdot \left( C_{\text{vs}} + \left( C_{\text{vs,max}} - C_{\text{vs}} \right) \cdot \text{Factor} \right)}{Q_s}$$

$$\text{With : } C_{\text{vs,max}} = \frac{Q_s}{Q_{1,\text{out}}} \quad \text{and} \quad C_{\text{vs,max}} < 0.5$$

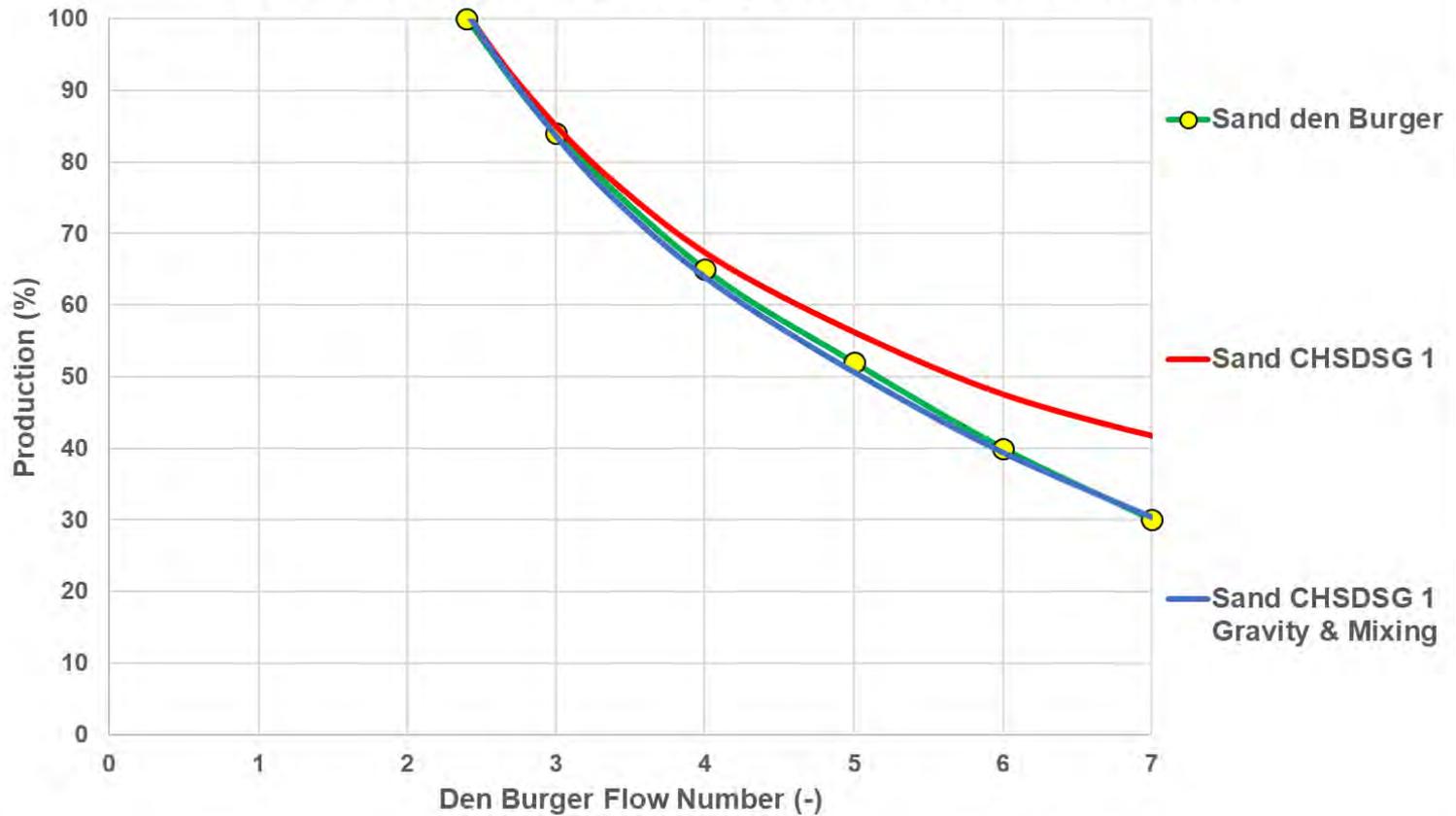
$$\text{Factor} = 0.1 \cdot \left( \frac{v_t \cdot \sin(\theta) \cdot \pi \cdot r_r^2}{Q_m} \right)^2 + \left( \frac{\text{Bu}}{10.8} \right)^3$$

$$\text{Factor} \leq 1$$

# Model versus Experiments in Sand



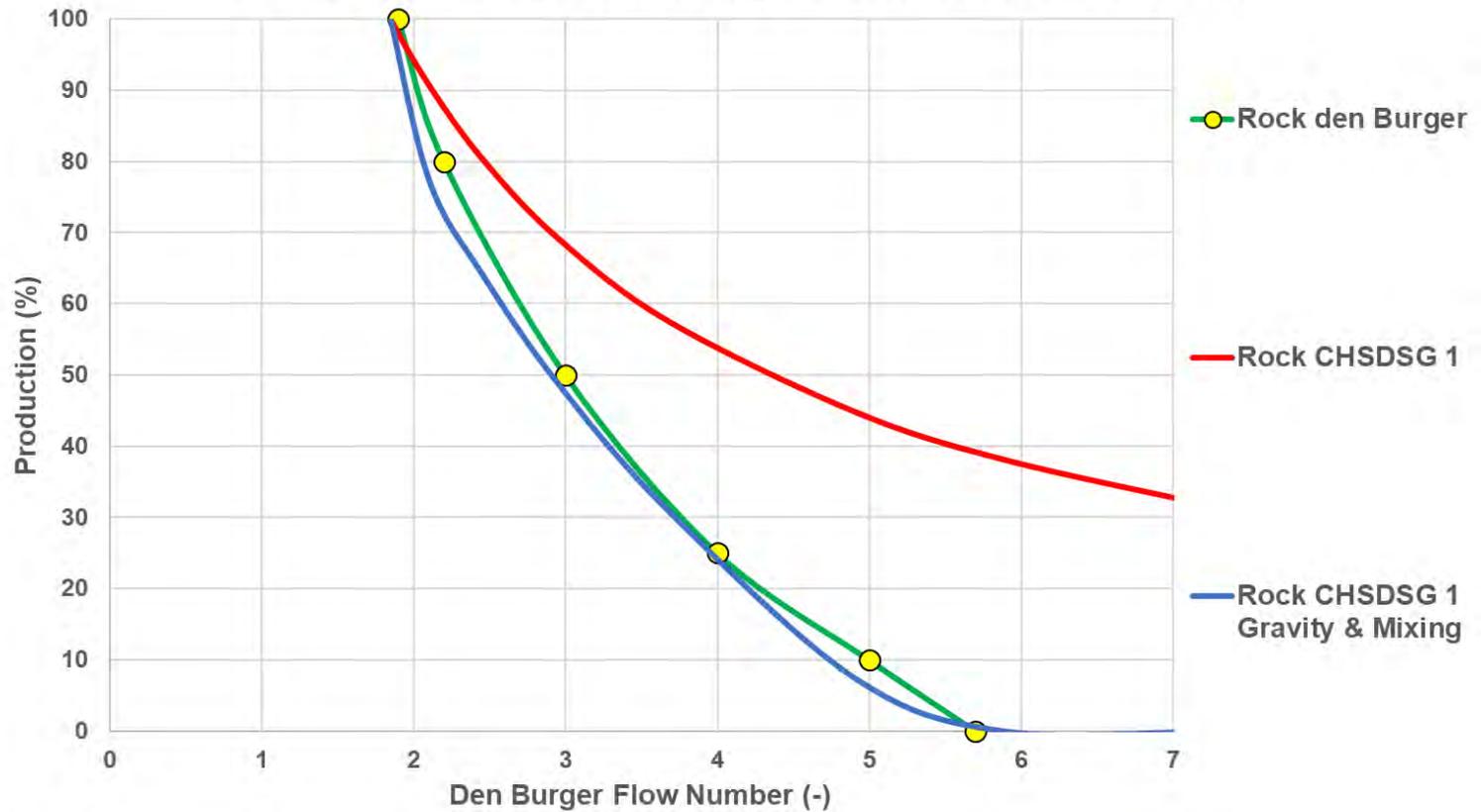
Production versus den Burger Flow Number in Sand



# Model versus Experiments in Rock



Production versus den Burger Flow Number in Rock





# Euler Equation Model

# Euler Equation

$$\Delta p_E = \rho_m \cdot u_o \cdot \left( u_o - \frac{Q \cdot \cot(\beta_o)}{2 \cdot \pi \cdot r_o \cdot w} \right) - \rho_m \cdot u_i \cdot \left( u_i - \frac{Q \cdot \cot(\beta_i)}{2 \cdot \pi \cdot r_i \cdot w} \right)$$

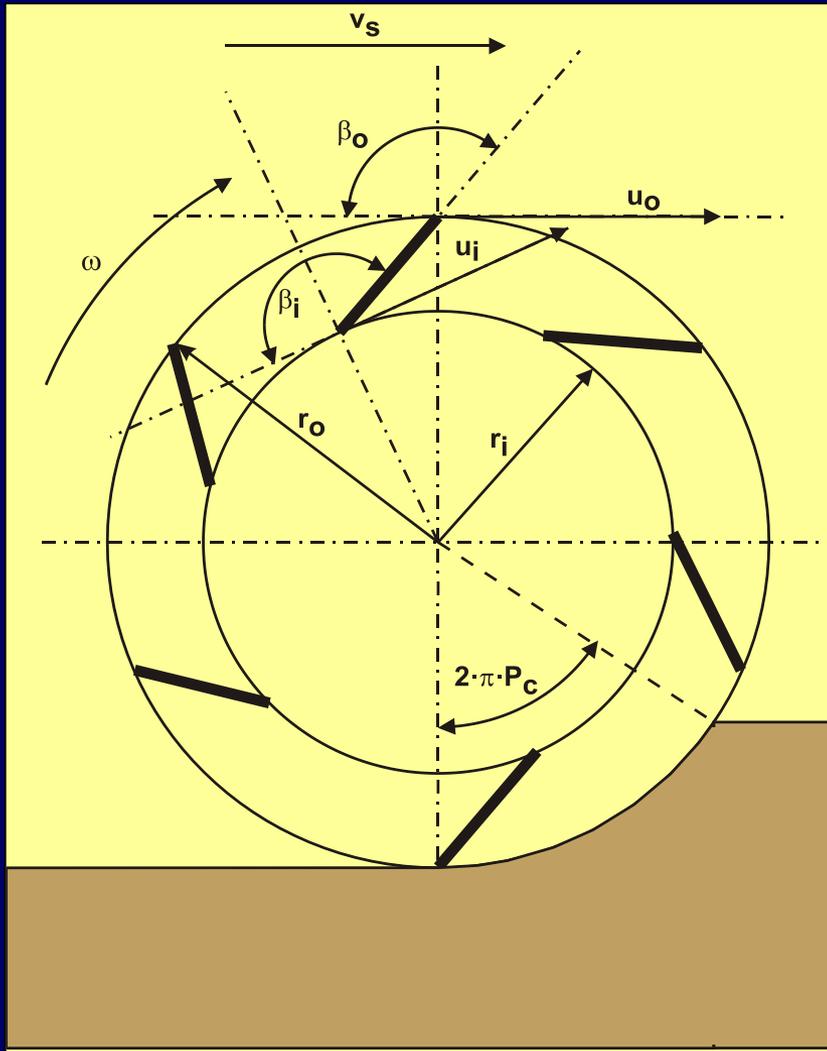
$$\Delta p_E = \rho_m \cdot \omega^2 \cdot (r_o^2 - r_i^2) - \frac{\rho_m \cdot \omega \cdot Q}{2 \cdot \pi \cdot w} \cdot (\cot(\beta_o) - \cot(\beta_i))$$

$$Q = \alpha \cdot 2 \cdot \pi \cdot \omega \cdot r_o^2 \cdot w$$

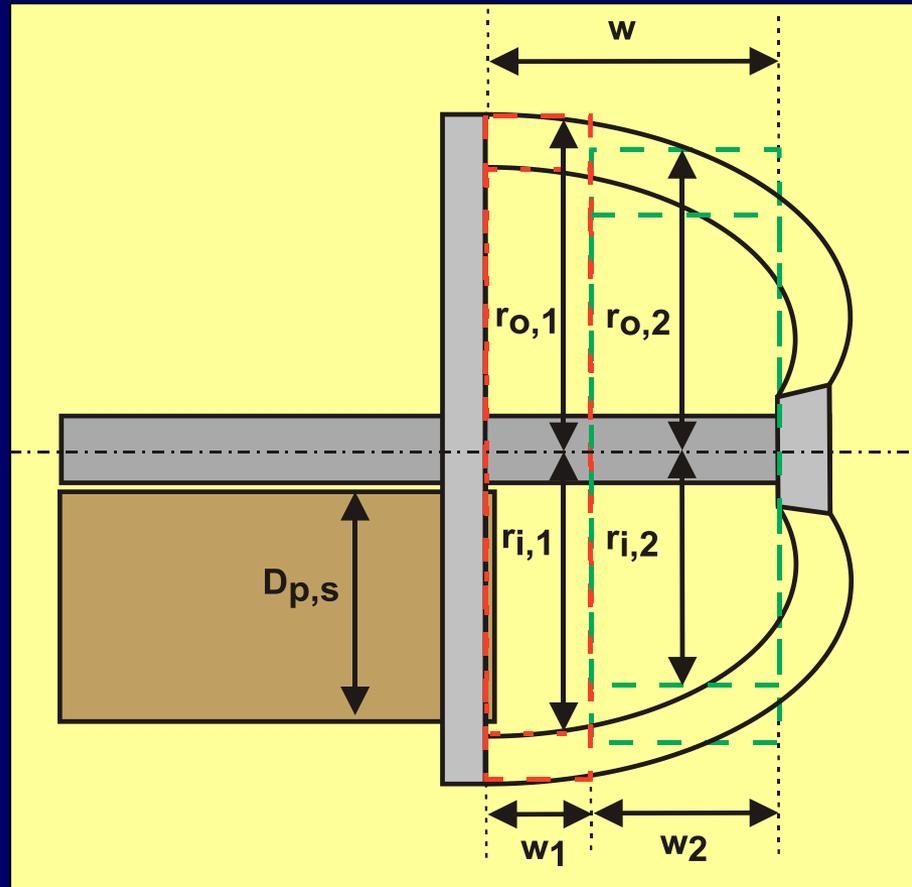
$$\Delta p_E = \rho_m \cdot \omega^2 \cdot (r_o^2 - r_i^2) - \alpha \cdot \rho_m \cdot \omega^2 \cdot r_o^2 \cdot (\cot(\beta_o) - \cot(\beta_i))$$

$$\Delta p_E = \rho_m \cdot \omega^2 \cdot \left( (r_o^2 - r_i^2) - \alpha \cdot r_o^2 \cdot (\cot(\beta_o) - \cot(\beta_i)) \right)$$

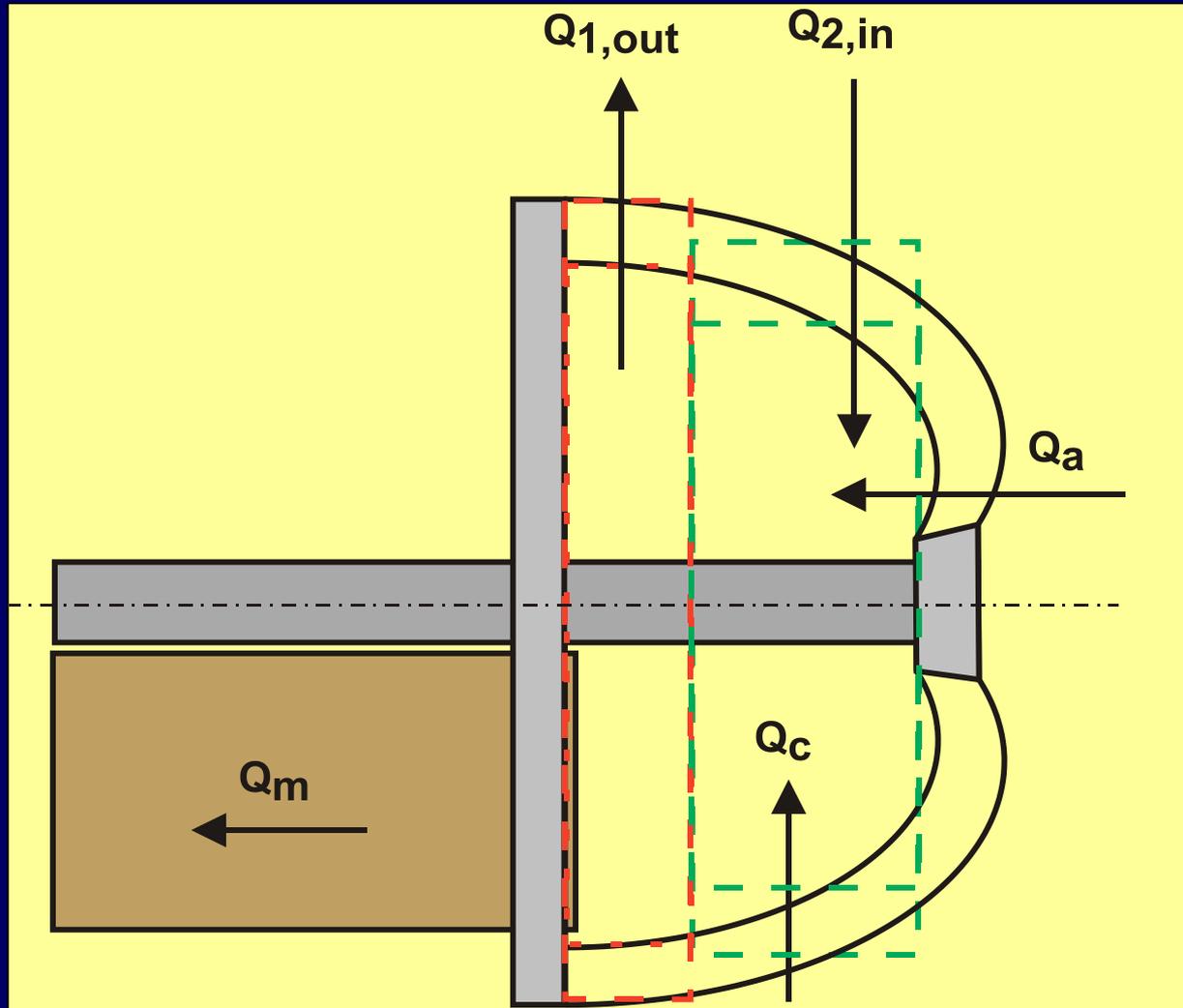
# Cutter Head Dimensions



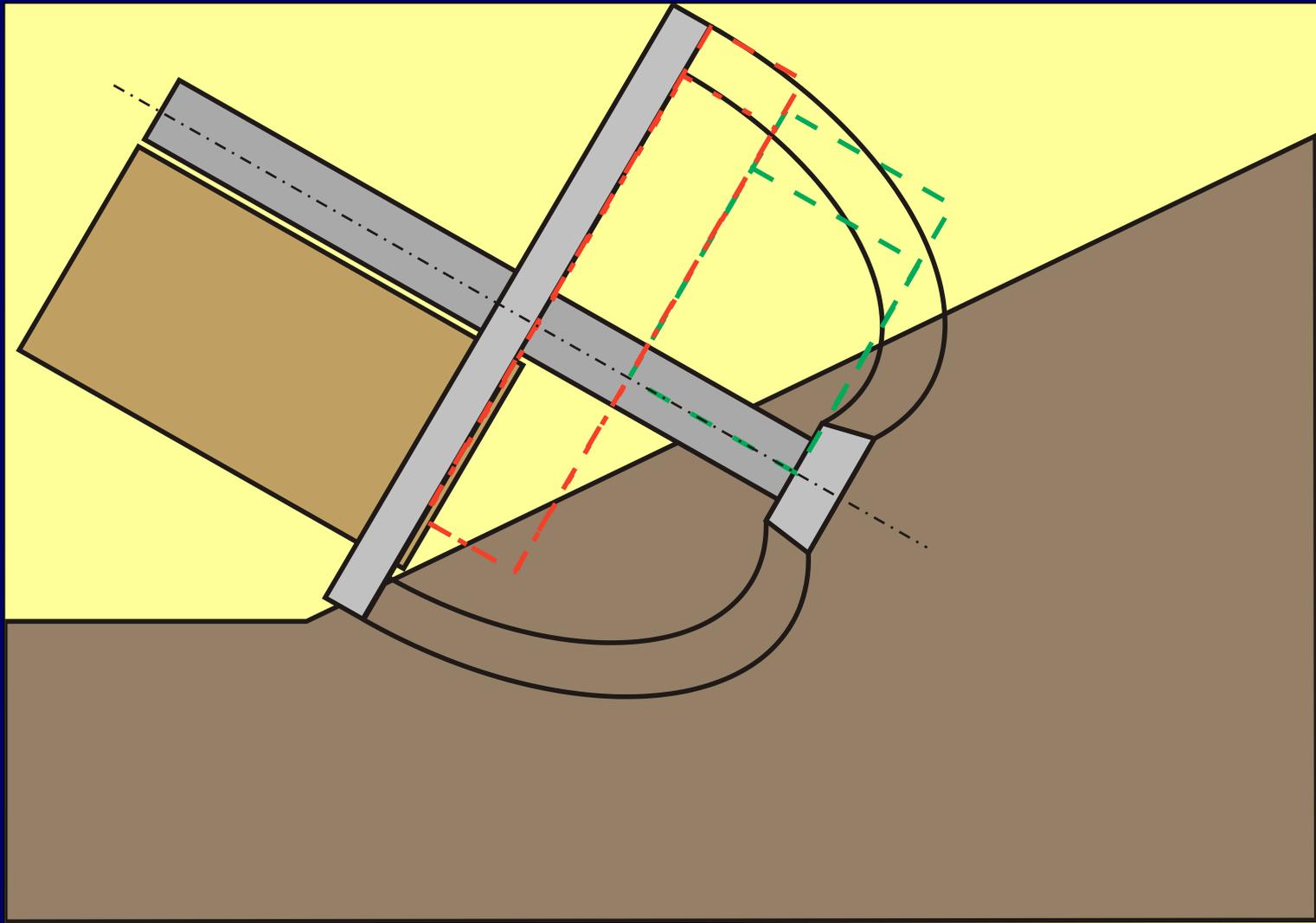
# Cutter Head Segments



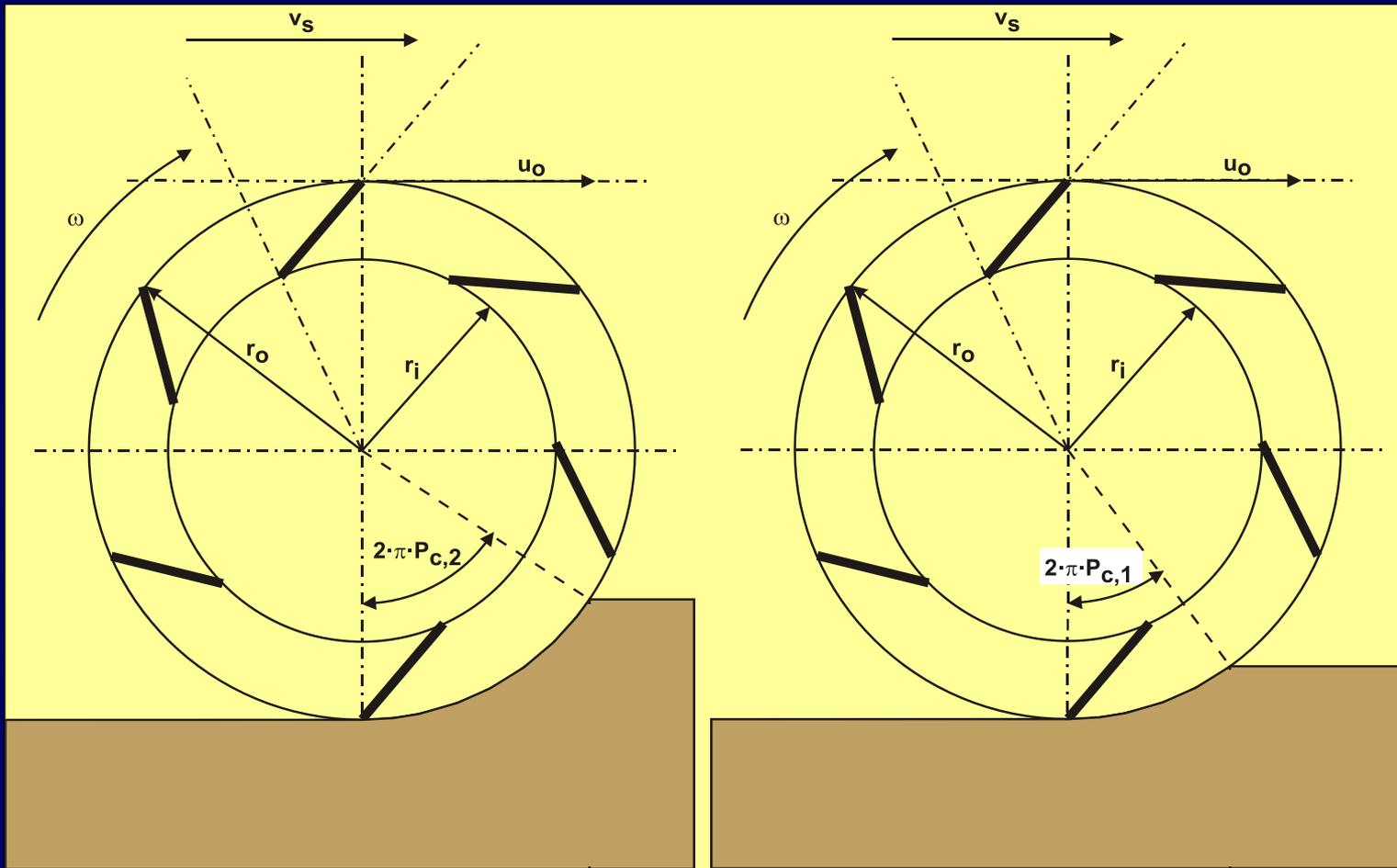
# The Flows in a Cutter Head



# The Cutter Head in the Bank



# The Cutter Head in the Bank



# Flows

$$Q_{1,\text{out}} = \alpha \cdot 2 \cdot \pi \cdot \omega \cdot r_{0,1}^2 \cdot (1 - P_{c,1}) \cdot$$

$$\left( \frac{f}{(1+f)} \cdot w - \frac{1}{(1+f)} \cdot \frac{1}{2 \cdot \pi \cdot \alpha \cdot \omega} \cdot \left( \frac{Q_m - Q_c - Q_a}{r_{0,1}^2 \cdot (1 - P_{c,1})} \right) \right)$$

$$Q_{2,\text{in}} = 2 \cdot \pi \cdot \alpha \cdot \omega \cdot (r_{0,1}^2 - r_{0,2}^2) \cdot (1 - P_{c,2}) \cdot$$

$$\left( \frac{1}{(1+f)} \cdot w + \frac{1}{(1+f)} \cdot \frac{1}{2 \cdot \pi \cdot \alpha \cdot \omega} \cdot \left( \frac{Q_m - Q_c - Q_a}{r_{0,1}^2 \cdot (1 - P_{c,1})} \right) \right)$$

# Spillage Non-Homogeneous

$$\text{Spillage} = \frac{Q_{1,\text{out}}}{Q_m + Q_{1,\text{out}}} = \frac{Q_{1,\text{out}} \cdot C_{\text{vs}}}{Q_s}$$

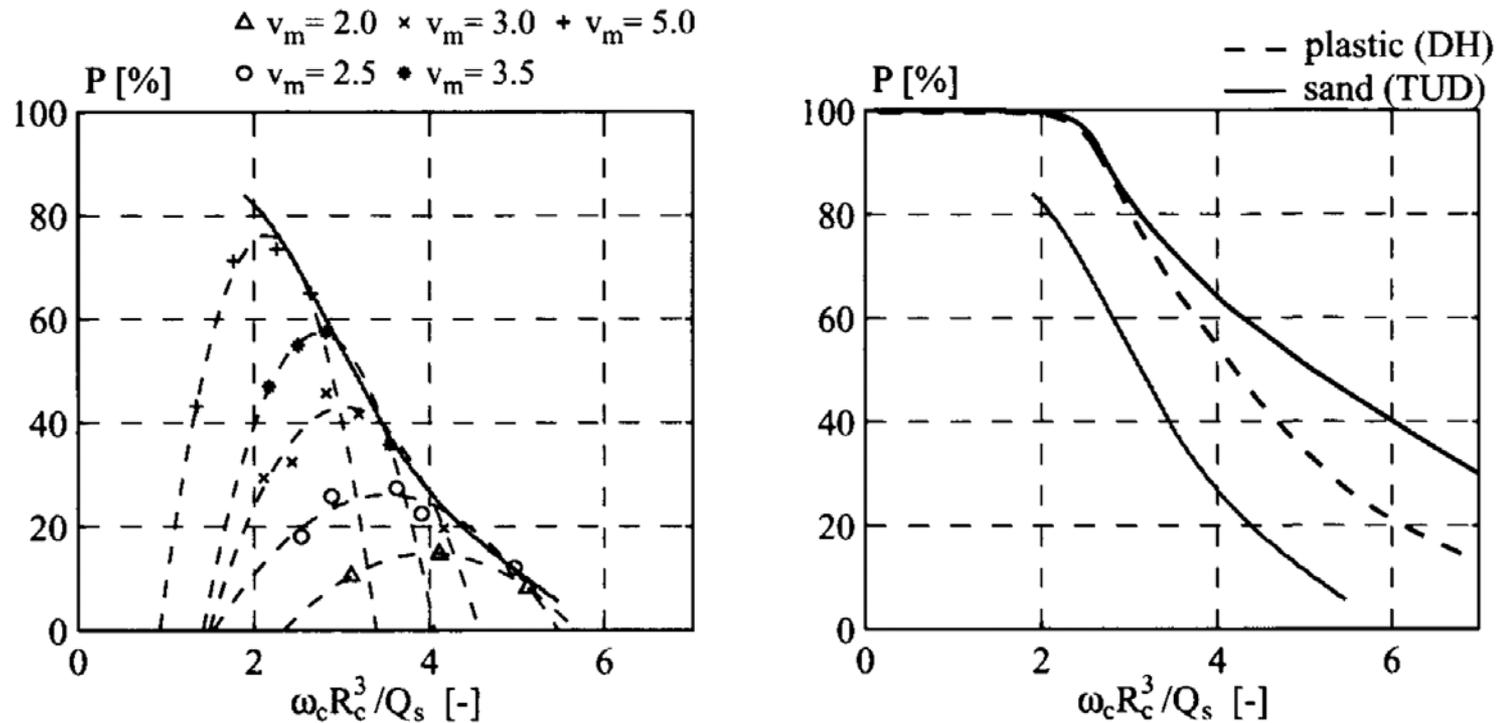
$$\text{Spillage} = \frac{Q_{1,\text{out}} \cdot \left( C_{\text{vs}} + \left( C_{\text{vs,max}} - C_{\text{vs}} \right) \cdot \text{Factor} \right)}{Q_s}$$

$$\text{With : } C_{\text{vs,max}} = \frac{Q_s}{Q_{1,\text{out}}} \quad \text{and} \quad C_{\text{vs,max}} < 0.5$$

$$\text{Factor} = 0.1 \cdot \left( \frac{v_t \cdot \sin(\theta) \cdot \pi \cdot r_r^2}{Q_m} \right)^2 + \left( \frac{\text{Bu}}{10.8} \right)^3$$

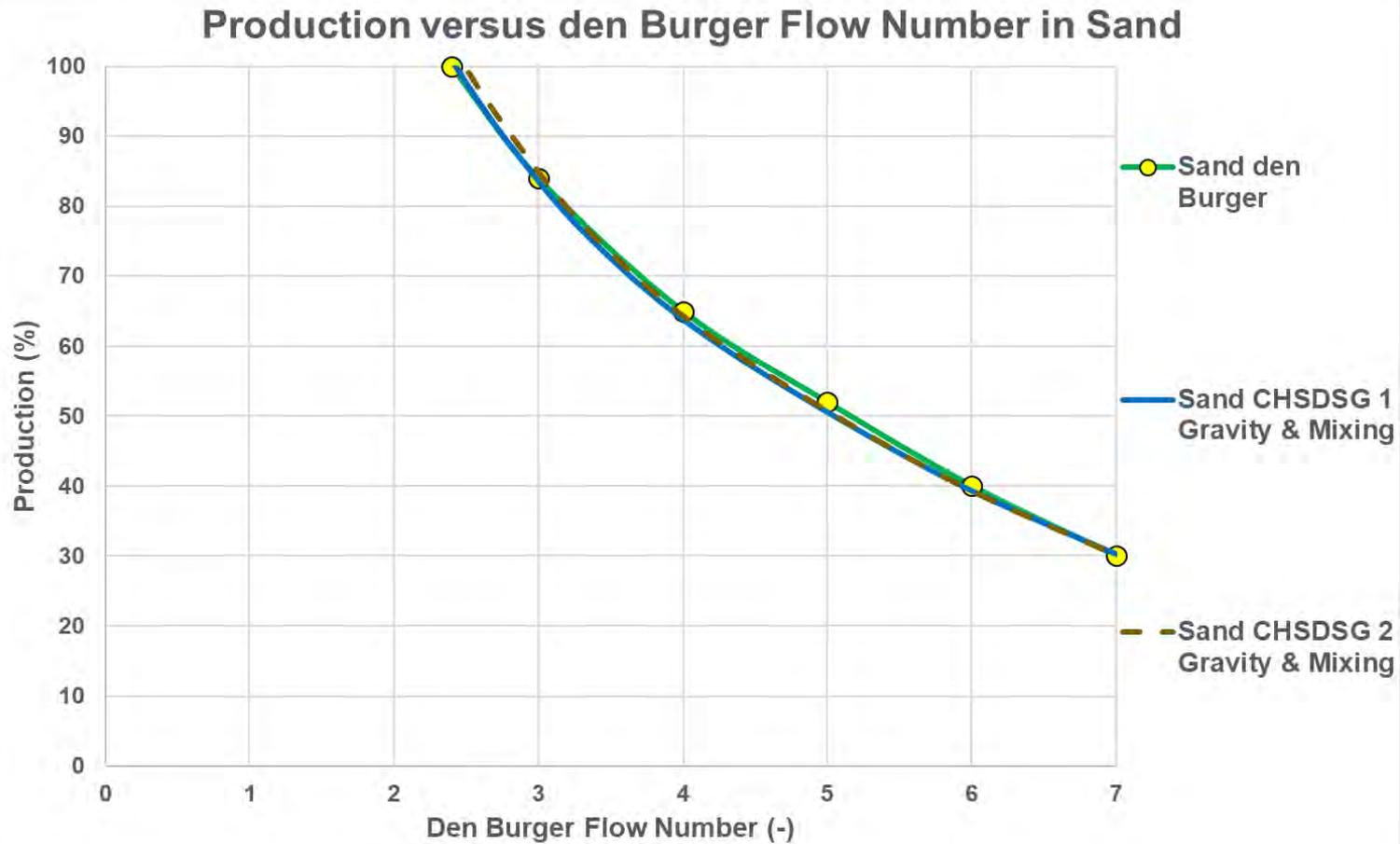
$$\text{Factor} \leq 1$$

# Production den Burger

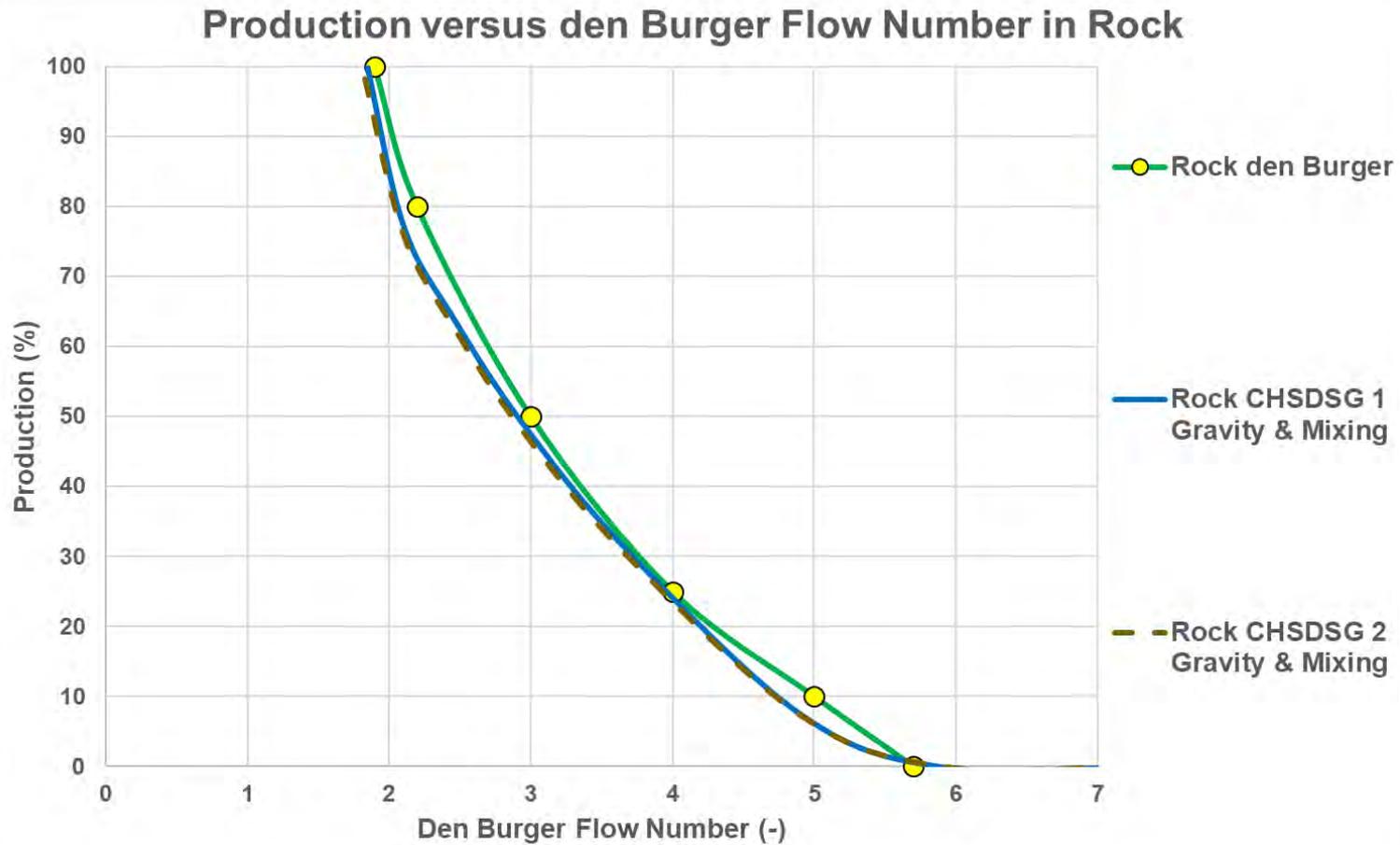


**Figure 6.7:** Production percentage vs. inverse of the flow number in the under-cut situation for cutting of gravel (left plot) and the results of the sand and plastic particles (right plot)

# Model versus Experiments in Sand



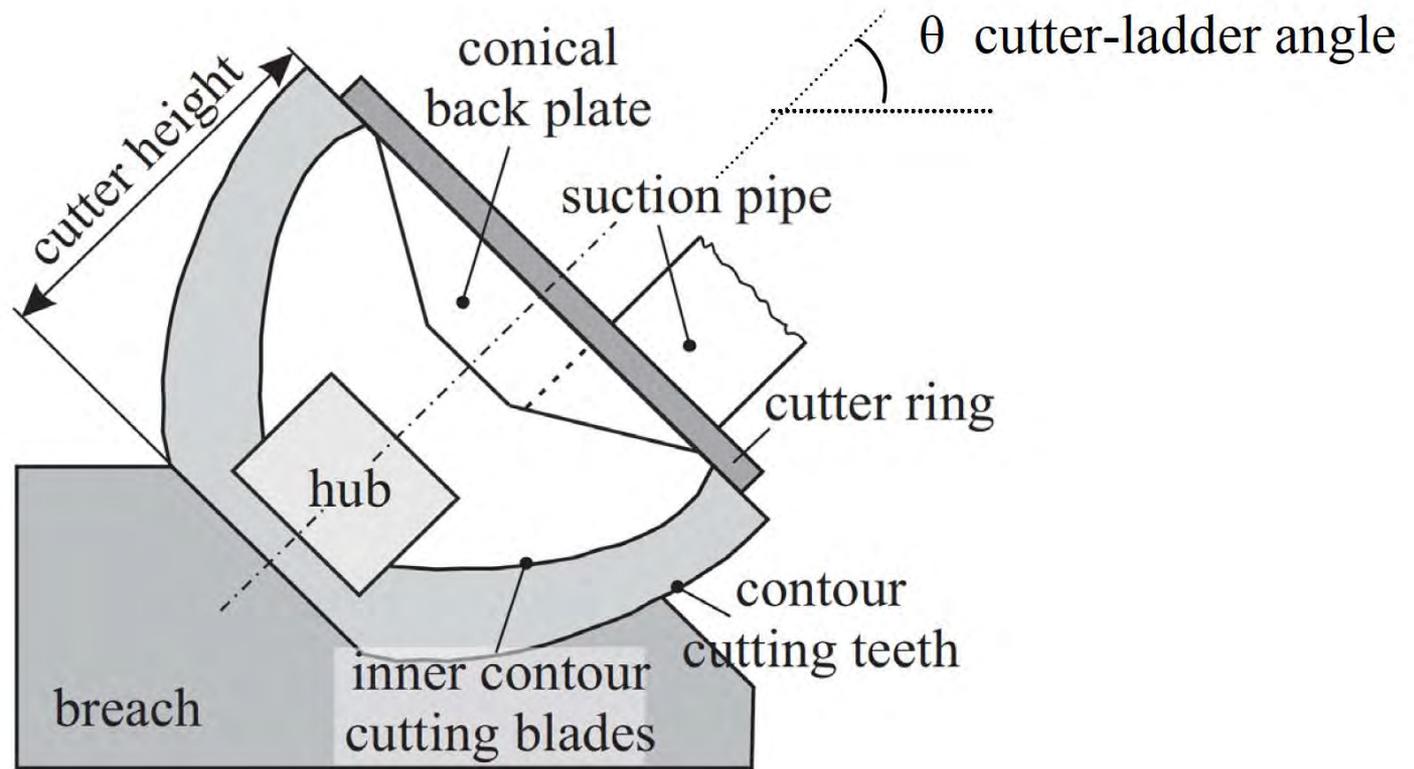
# Model versus Experiments in Rock





# Filling Degree

# Filling Degree



**Figure 2. Model cutter positioned in breach.**

# Filling Degree

$$\text{FillingDegree} = \xi \cdot \left( \frac{D_r \cdot 2 \cdot \pi \cdot n \cdot \cos(\theta)}{2 \cdot 60 \cdot v_t} \right)^2$$

and

$$\text{FillingDegree} \leq 1$$

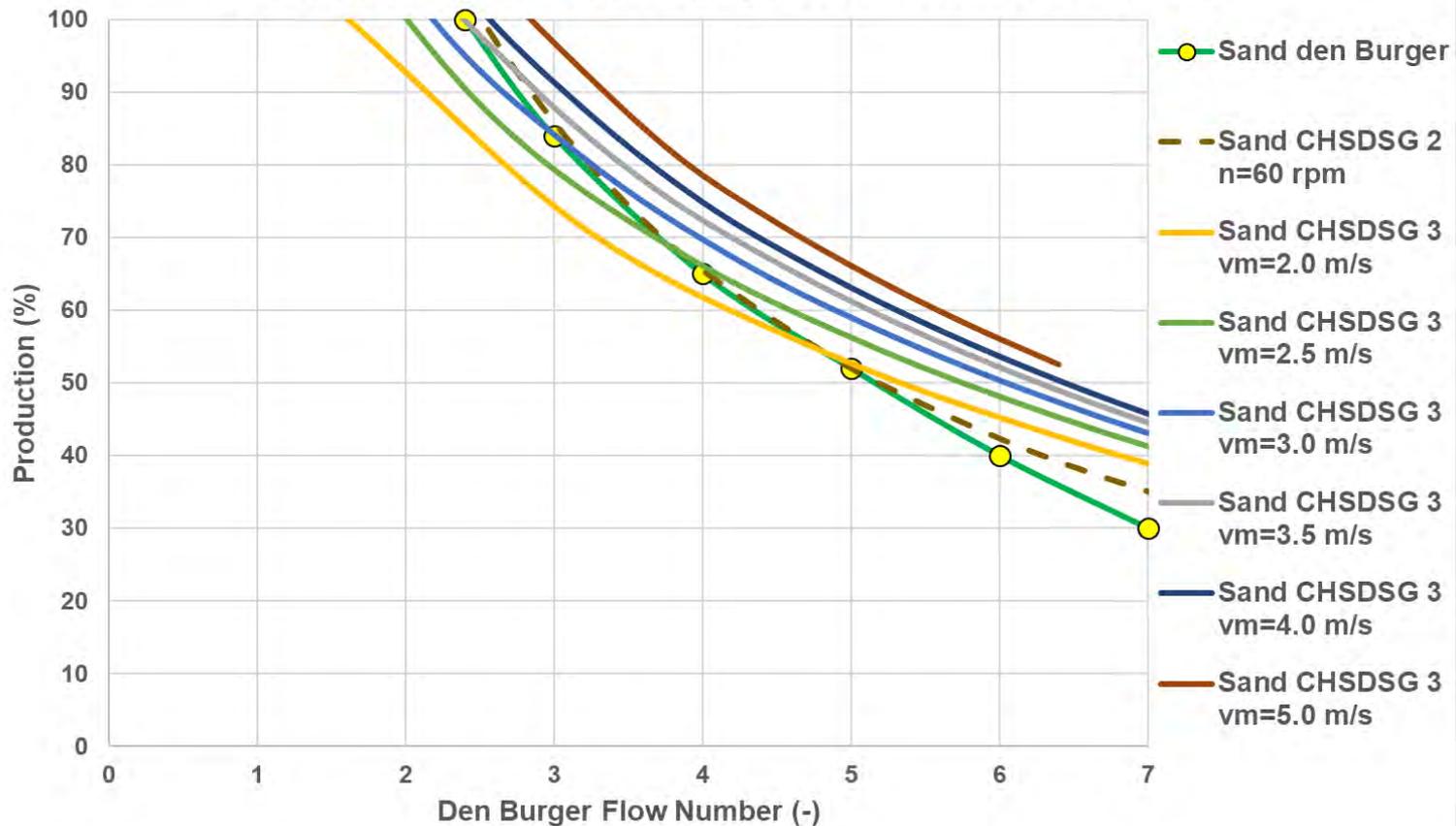
$$\text{FinalSpillage} = \text{Spillage} \cdot \text{FillingDegree} + (1 - \text{FillingDegree})$$



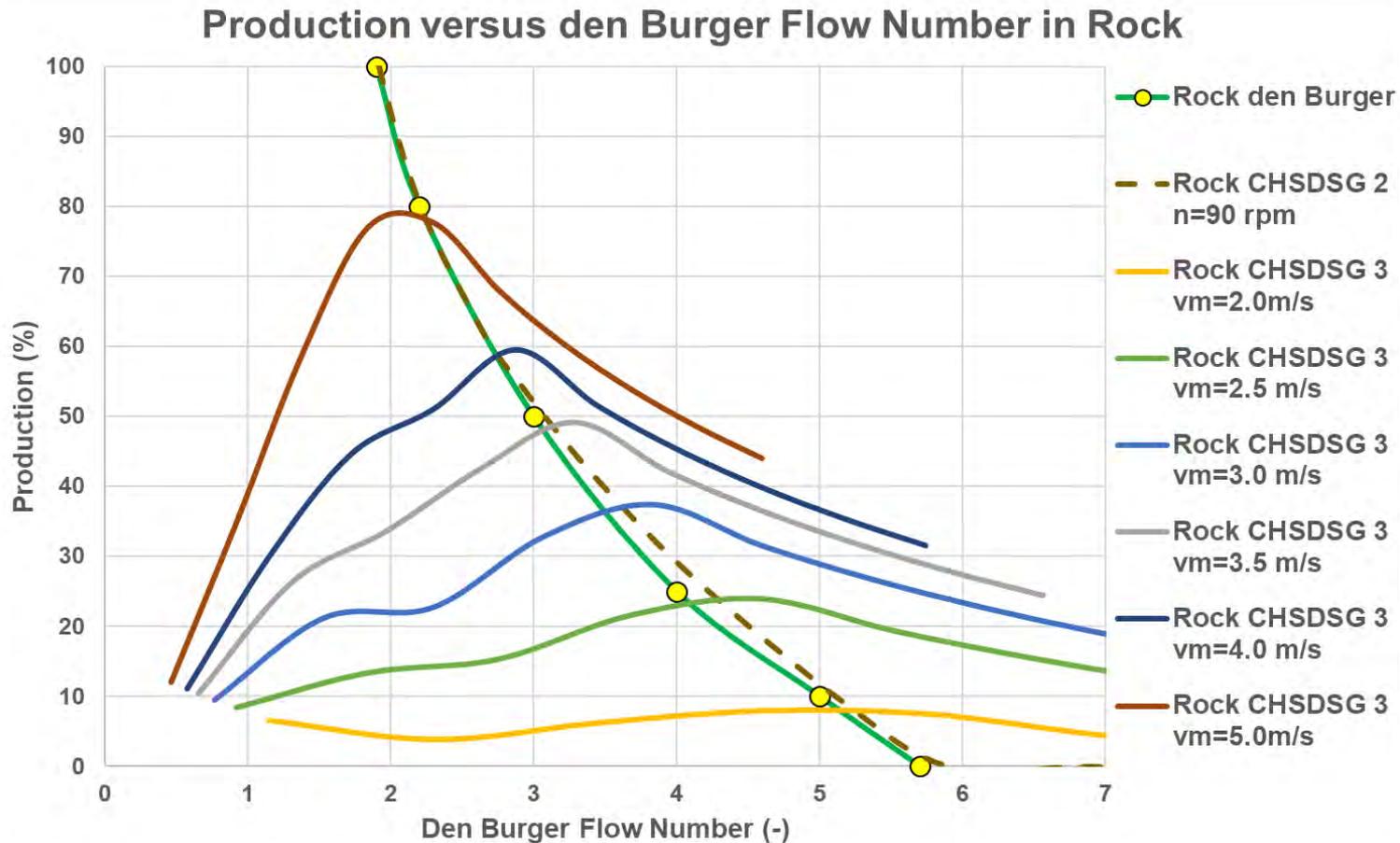
# Filling Ratio in Sand



Production versus den Burger Flow Number in Sand



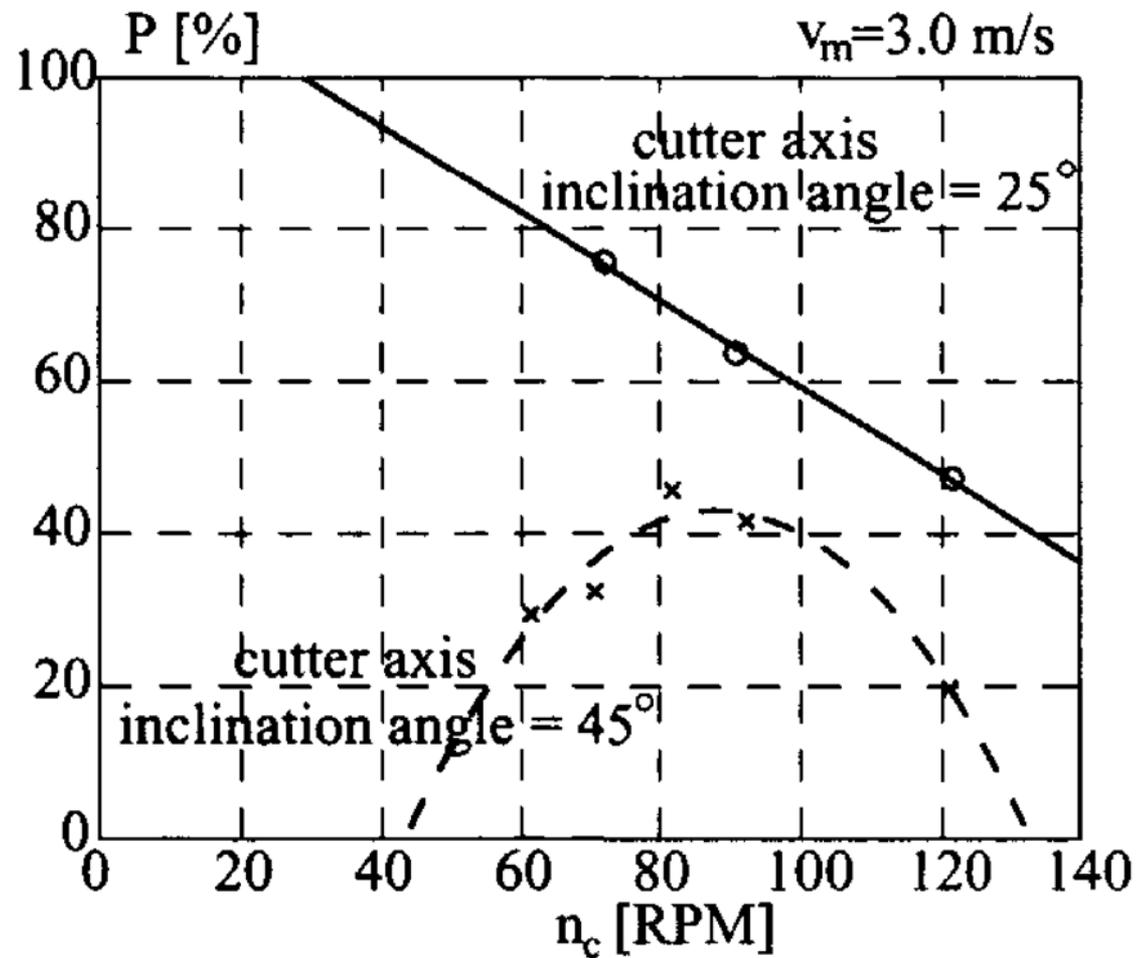
# Filling Ratio in Rock





# Ladder Angle

# Ladder Angle



# Ladder Angle Influence

$$\text{Spillage} = \frac{Q_{1,\text{out}} \cdot \left( C_{\text{vs}} + (C_{\text{vs,max}} - C_{\text{vs}}) \cdot \left( 0.1 \cdot \left( \frac{v_t \cdot \sin(\theta) \cdot \pi \cdot r_r^2}{Q_m} \right)^2 + \left( \frac{Bu}{10.8} \right)^3 \right) \right)}{Q_s}$$

$$\text{FillingDegree} = \xi \cdot \left( \frac{D_r \cdot 2 \cdot \pi \cdot n \cdot \cos(\theta)}{2 \cdot 60 \cdot v_t} \right)^2$$

and

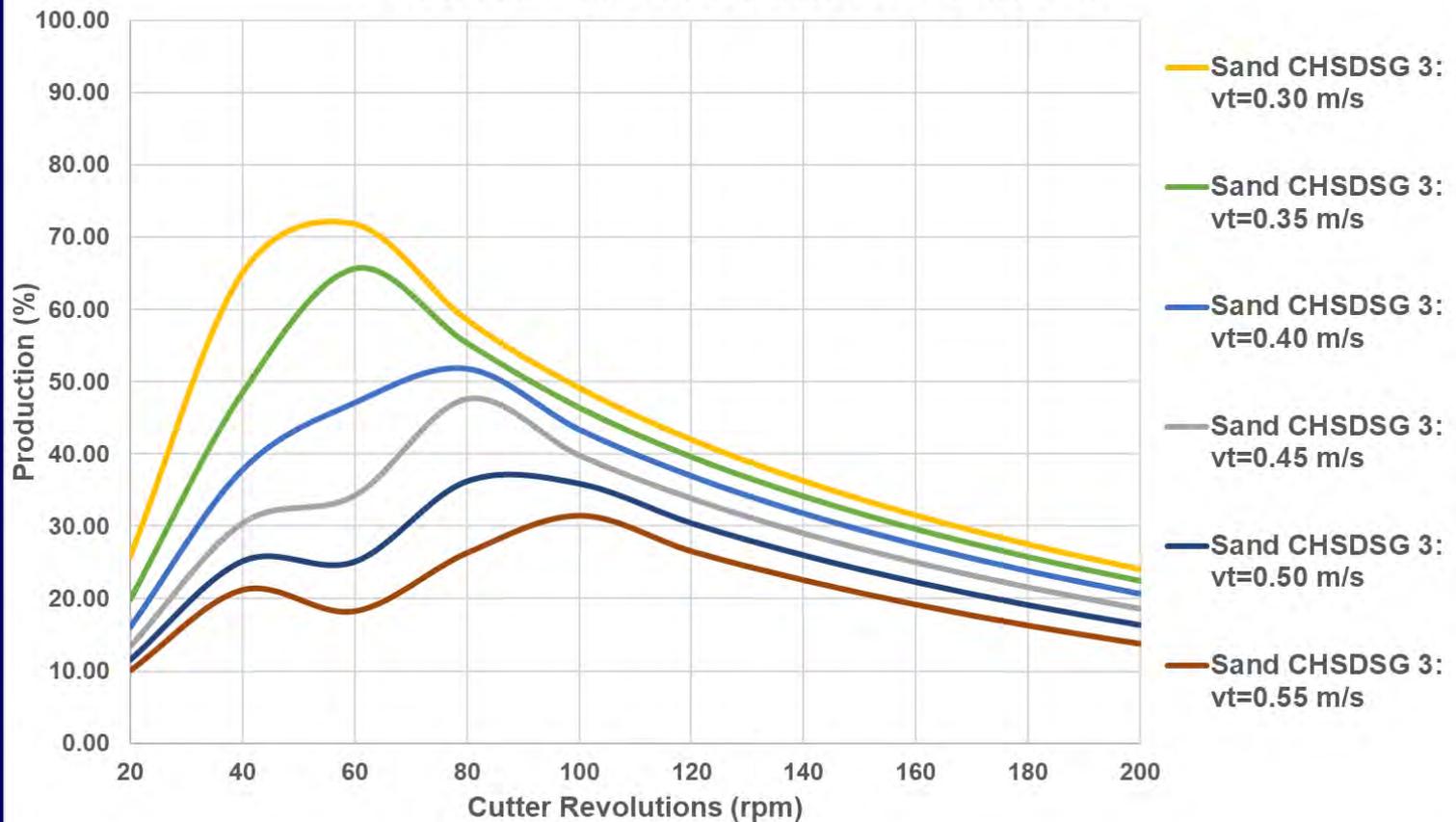
$$\text{FillingDegree} \leq 1$$

$$\text{FinalSpillage} = \text{Spillage} \cdot \text{FillingDegree} + (1 - \text{FillingDegree})$$

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# Ladder Angle 45°

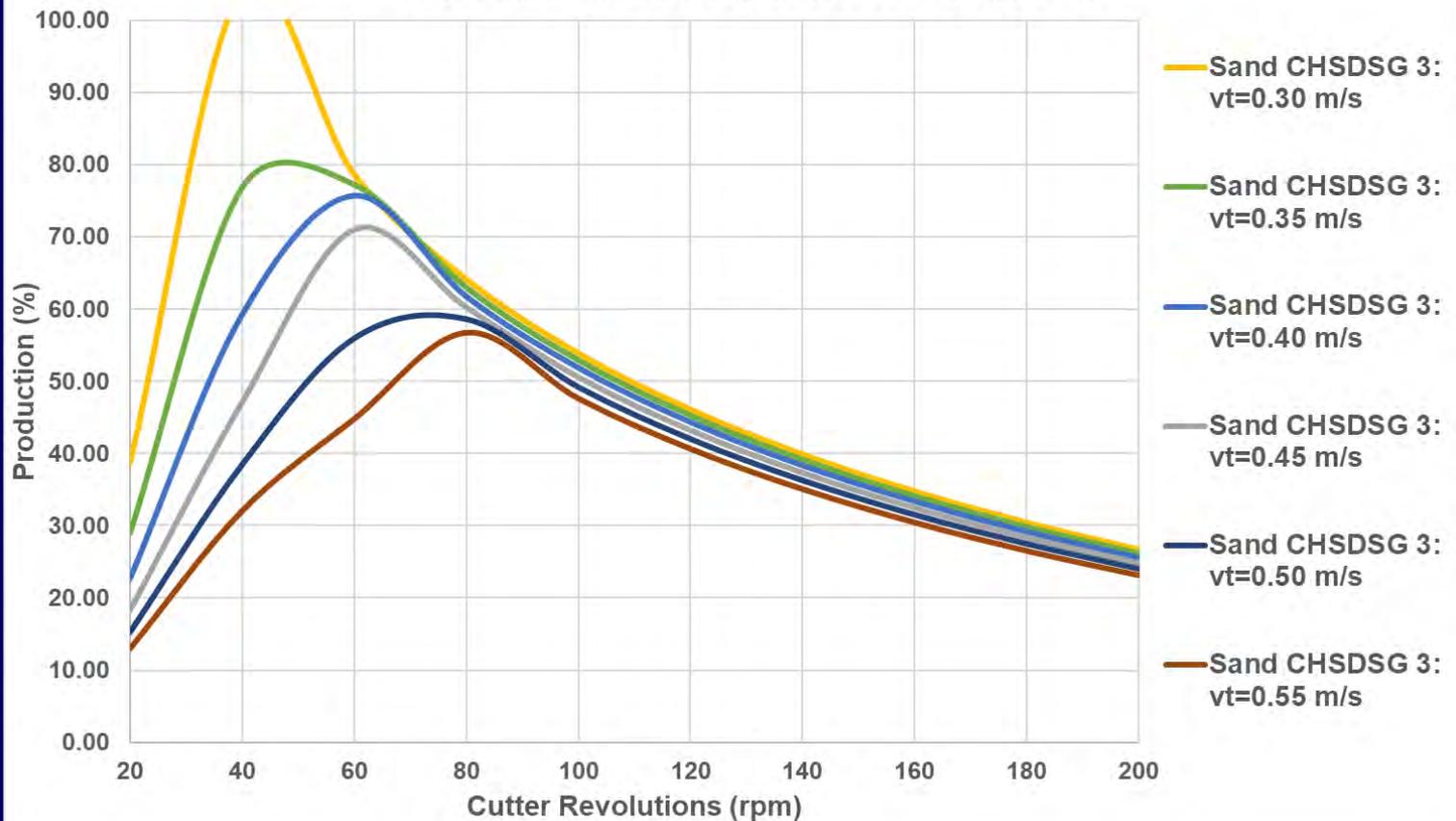
## Production versus Cutter Revolutions



# Ladder Angle 25°



## Production versus Cutter Revolutions





# Validation Miltenburg 1983

# The 40 cm Model Cutter Head for Rock



# Configurations

Miltenburg (1982) used 6 different configurations of the crown cutter head and of course carried out the experiments overcutting and undercutting. The 6 configurations are:

- No skirts, short cone, suction mouth at  $0^\circ$ .
- No skirts, long cone, suction mouth at  $0^\circ$ .
- No skirts, long cone, suction mouth at  $+30^\circ$ .
- No skirts, long cone, suction mouth at  $-30^\circ$ .
- Skirts, long cone, suction mouth at  $0^\circ$ .
- Skirts, long cone, suction mouth at  $+30^\circ$ .

Besides the 6 configurations, each test has been carried out overcutting and undercutting. So, many subsets of experiments can be made.

# The Cone and the Short Cone

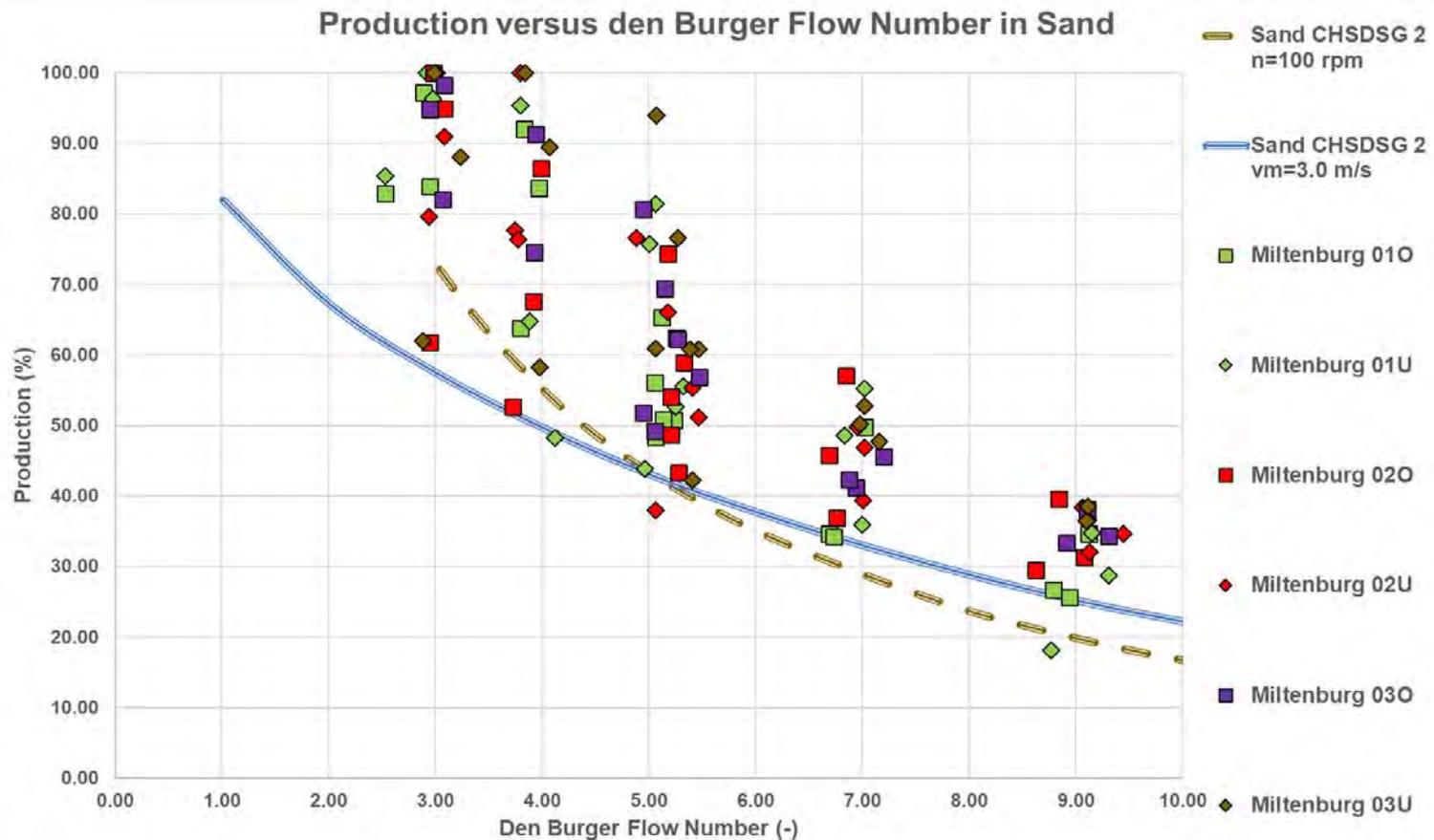


# Skirts Inside the Cutter Head



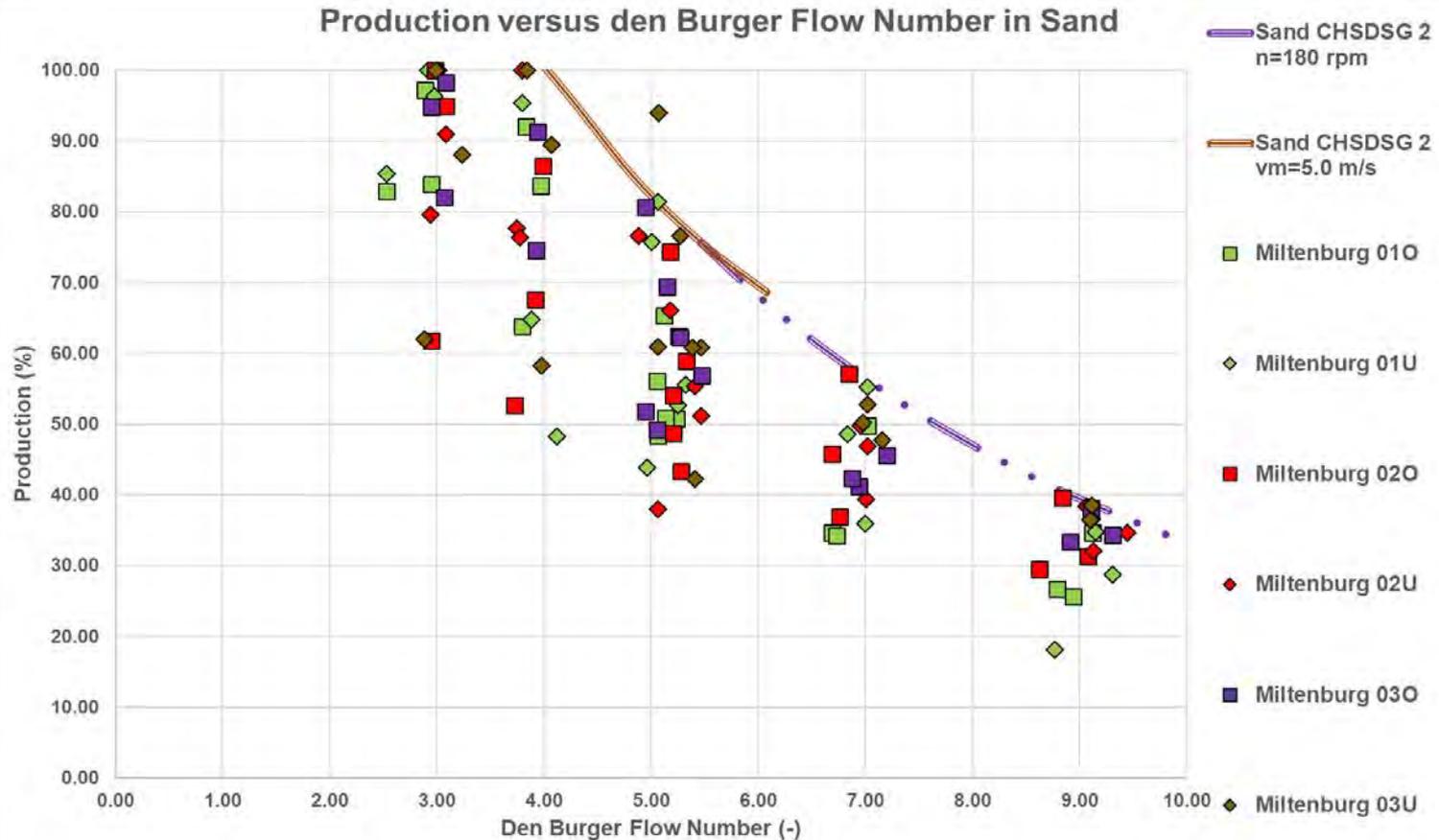


# Data Miltenburg with Lower Limit



The lower limit is determined from  $n=100$  rpm and  $v_m=3$  m/s. No skirts, suction mouth normal.

# Data Miltenburg with Upper Limit



The upper limit is determined from  $n=180$  rpm and  $v_m=5$  m/s. No skirts, suction mouth normal.

# Conclusions

- An analytical model has been derived and validated.
- The ratio of the rotating volume flow inside the cutter head to the mixture flow gives a useful dimensionless number named the Burger number.
- Below a certain Burger number there is no spillage, so the total flow into the cutter head equals the mixture flow into the suction mouth.
- Above this Burger number, the spillage increases non-linear. The higher the Burger number the smaller the increase of the spillage.
- The Miltenburg data indicate the spillage does not reach 100% at very high Burger numbers.
- Terminal settling velocity of the particles and ladder angle play an important role in the spillage model.

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# Conclusions Final Equation

$$\text{Spillage} = \frac{Q_{1,\text{out}}}{Q_m + Q_{1,\text{out}}} = \frac{Q_{1,\text{out}} \cdot C_{vs}}{Q_s}$$

$$\text{Spillage} = \frac{Q_{1,\text{out}} \cdot \left( C_{vs} + \left( C_{vs,\text{max}} - C_{vs} \right) \cdot \text{Factor} \right)}{Q_s}$$

$$\text{With : } C_{vs,\text{max}} = \frac{Q_s}{Q_{1,\text{out}}} \quad \text{and} \quad C_{vs,\text{max}} < 0.5$$

$$\text{Factor} = 0.1 \cdot \left( \frac{v_t \cdot \sin(\theta) \cdot \pi \cdot r_r^2}{Q_m} \right)^2 + \left( \frac{\text{Bu}}{10.8} \right)^3 - \left( \frac{\text{Bu}}{12} \right)^4$$

$$\text{Factor} \leq 1$$



Questions?